FLOW OVER LONGITUDINAL BAR BOTTOM-RACKS

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for the Degree of

MASTER OF TECHNOLOGY

by SHREE KANT SHUKLA

to the

DEPARTMENT OF CIVIL ENGINEERING

INDIAN INSTITUTE OF TECHNOLOGY, KANPUR

APRIL, 1987

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My Father and Late Mother

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Dated: April 15, 1987

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(Shree Kant Shukla)

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NOTATIONS

```
В
      Width of rack = Width of flume
      Coefficient of discharge through the rack (= \frac{D}{BLE/2g E_0})
C_{\mathbf{d}}
      Diameter of rack bars
D
Е
      Specific energy of the flow at a section
E
      Total energy loss over the rack
F
      Froude number of the flow at a section
L
      Abstraction length of the rack
N
      Number of bars in the rack
      Diverted flow through the rack
Q_{\mathbf{n}}
      Residual flow in the flume
Q_{R}
Q_{S}
       Total flow of the approaching stream
      Diverted discharge per unit length of the rack
q.
R_{eo}
      Reynolds number of the flow at section (0)
^{
m R}_{
m er}
      Reynolds number of the flow through the rack
S
      Clear spacing between rack bars
Sh
      Submergence of the inlet
       Energy slope along the rack
Se
       Temperature of water in degree centigrates
T
V
      Mean velocity of the flow
       Resultant average velocity of flow through rac
V_{r}
       Depth of flow at beginning of the rack
Yle
       Depth of flow at end of the rack
Y2e
       Critical depth of approach flow
Yc
       Downstream critical depth
y_{c1}
       Depth of approach flow (at section (0))
λ
      Liminting inlet depth of flow
Y11.
      Opening area ratio of the rack (1-ND/B)
6
```

Kinematic viscosity of water.

V(Nu)

ABSTRACT

An experimental study of the hydraulic behaviour of longitudinal bar bottom-racks for different flow conditions and geometry of the rack has been carried out. The flow has been classified into five types viz, Al, A2, A3, Bl and B2, based on the approach flow condition and the effect of the tail water at the inlet. The Al, A3, and Bl flows have been studied in detail in the present work. The variation of the limiting inlet depth ratio with the opening area ratio of the rack has been determined in Al and Bl flows and enables one to predict whether the flow over the rack is fully submerged or not. A suitable coefficient of discharge has been defined by using a working specific energy head and the orifice type of flow. Important flow and rack parameters affecting the coefficient of discharge C_d have been identified. The flow parameter in Alflows was found to have negligible effect on C_d , while it has considerable effect in A3 and B1 flows. The variation of the discharge diversion in a rack has also been studied with pertinent flow and rack parameters for Al and Bl flows separately.

The energy loss was found to be substantial particularly in Al and Bl flows, though it was negligible in A3 flows. The energy slope over the rack has been studied with prominent flow and rack parameters and approximate relationships have been obtained for evaluating the energy slope in

Al and Bl flows. This information will be useful in realistic estimation of water survatace profiles over a rack.

The findings of the present study provides basic data for effective and rational design of trench weirs.

. CHAPTER I

INTRODUCTION

1.1 Bottom-Racks and Their Applications:

Hydraulic structures are used to utilise effectively the available water-resources. Plans for the development of water-resources demand improved performance of hydraulic structures to harness river waters. Bottom-racks, also called as bottom-intakes, are hydraulic structures used to divert the flow in open-channels. Such bottom-intakes find diverse applications in different fields of hydraulic engineering, particularly in diverting water from mountanous streams. Some of the applications of bottom intakes are listed below.

(1) An application of bottom-intake which is becoming more popular nowadays because of the economy in it's use as horizontal trash racks in the hydro-power plants located on mountanous streams. Such a structure, besides being simple in construction, eliminates the possible damage during floods to which any raised crest across the streams used for flow diversion would be susceptible.

Such bottom-intakes in the streams are also known as '' Trench Weirs''. Some of the trench weir installations in India are:

(i) Two components of Binwa Hydroelectric project (H.P.) 2x3MW.

- (ii) Andhra Hydroelectric project (H.P.) 3x5.65MW.
- (iii) Bhaledh Nallah component of Baira-Siul Hydel Project 3x60 MW.
- (iv) Stakna Hydel project, Leh (J and K).

Detailed information on Trench Weirs are available in Ref. (2,9).

- (2) In an irrigation canal system the surface runoff may some times be let into a canal and excess flow may be disposed off at some convenient location downstream to a suitable drainage. The bottom-racks can effectively be used for this purpose.
- (3) A very common use of bottom-racks is as '' Kerb-outlets' on the sides of main street to drain storm water into the subsurface drains. These outlets may be made up of horizontal or slightly inclined bottom racks.
- (4) Often, the bottom-racks are used as '' Skimmers '' when it is desired to reduce the volume of water to transport fish (1).
- (5) Bottom-rack can also be used in the sedimentation tanks to trap the debris in the grit chambers (11).
- (6) A bottom-intake structure designed for the use by the Government of Hong Kong to divert water from streams draining the Sai Kung Peninsula by a system of shafts and tunnels to a reservoir at high island is described in Ref.(14).

1.2 Different Kinds of Bottom-Racks:

Fig. 1.1 shows a typical definition sketch of a bottom-rack assembly. The bottom-racks can be classified into four categories on the basis of the nature of the rack as:

(i) Transverse bar bottom-racks:

In these racks the bars are placed transverse to the direction of flow. The bars may be of circular, rectangular or of any special shape to meet the specific requirement. When the width of the stream is large compared to the length of rack, the installation of these racks may sometimes prove to be uneconomical because of the requirement of too lengthy bars.

(ii) Longitudinal bar bottom-racks:

In these racks the bars are laid parallel to the direction of flow. The bars are of any convenient shape. These racks are convenient to install under field conditions, where the width of the stream is large compared to the length of the rack. All the trench weirs adopt this type of bottom-racks.

(iii) Perforated plate bottom-racks:

Such racks are generally used in process industries,
These are plates having uniformly spaced or staggered circular
holes.

(iv) Slots:

Slots are the limiting case of bottom-racks with all the bars removed.

Further to the above classification the bottomracks may be horizontal or inclined with reference to approach bed level of the channel.

The present investigation is confined to the study of horizontal longitudinal bar bottom-racks with circular bars only.

1.3. Hydraulics of Longitudinal Bar Bottom-Racks:

The flow over the bottom-rack is a spatially varied flow with decreasing discharge. The performance of a bottom rack depends upon the flow characteristics such as the amount of main flow, the state of flow approaching the rack and the geometric characteristics of the rack such as it's length, width, slope and the shape, width and spacing of the rack elements.

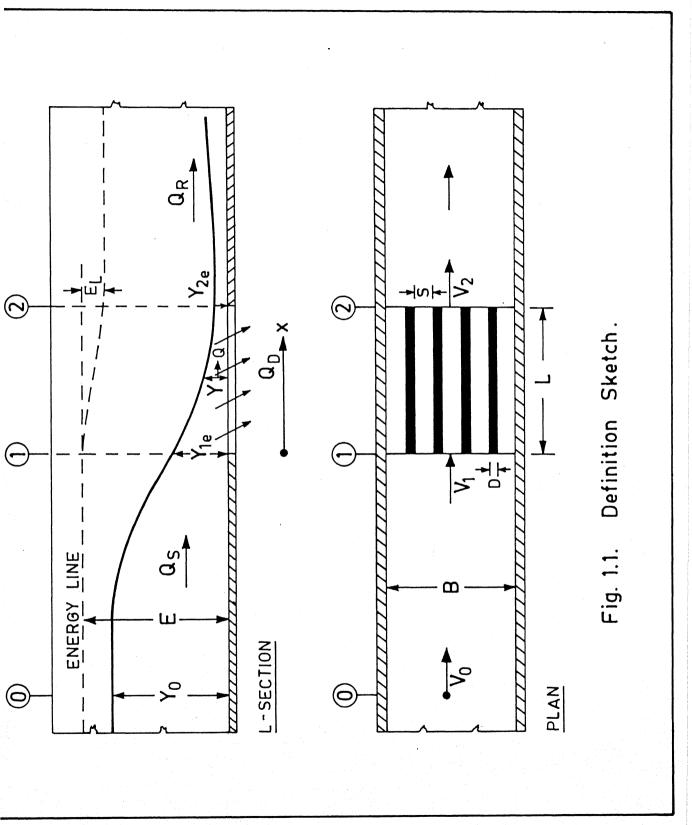
Fig. 1.1 is a definiton sketch of the flow over a horizontal longitudinal bar bottom-rack. The bars are made of circular rods of diameter D. The main variables involved in the problem are:

(a) Flow characteristics:

Rate of approach flow ${\bf Q_S},$ rate of diverted flow through the rack ${\bf Q_D},$ state of approach flow, depths ${\bf y_o}, {\bf y_{le}}$ and ${\bf y_{2e}}.$

(b) Geometry of the Rack:

This includes the length L, width B of the rack, the bar diameter D. and clear spacing S between bars.



(c) The fluid properties:

Chiefly the dynamic viscosity μ and mass density Q of water.

The basic hydraulic characteristics required to be predicted are:

- (i) To classify the different types of flows over the rack.
- (ii) A suitably defined coefficient of discharge C_d and it's variation.
- (iii) The diversion ratio Q_D/Q_S of the rack.
- (iv) The water-surface profile over the rack.
- (v) The energy loss over the rack.

The above information will help one to design such a bottom-intake with help of known parameters.

1.4 The Present Study:

A study of the relevant literature on the topic of bottom-racks indicated that this field has received very little attention compared to it's practical importance. The available works while meagre are essentially for the slots (4,6,11,13) and transverse bar racks (7,8,10). The case of longitudinal bar bottom-racks while being important from practical point of view, has not received due attention and the studies are limited to a few exploratory investigations (3,5,14).

Keeping in mind the unsatisfactory information available, an experimental study, to prodict the hydraulic behaviour of horizontal longitudinal bar bottom-racks made up of circular bars, was designed to get maximum possible useful information within the limitations of available time. The present study includes different approach flow conditions and geometries of the rack. Some of the related works available in the literature have been compared with the data of present study. The arrangement of different topics in the thesis is as follows:

A critical review of the available literature has been presented in Chapter II. Chapter III contains the details of experiments and observations. Analysis of the data collected in the present study is given in Chapter IV. The various conclusions arising out of the present study have been collected in Chapter V. Certain recommendations for further studies on this topic are also listed in this Chapter.

Appendix I contains the basic as well as derived data of the present study. All the data are given in a convenient tabular form. In Appendix II a design procedure for a bottom-intake has been explained. A simple Fortran program has also been given for designing such a bottom-intake in practical situations where the approach flow conditions and the rate of flow to be diverted from the intake are known. A worked example also has been given by taking the data from model studies of Banu and Parai Khads of Himanchal Pradesh and results have been compared with their original recommended design.

CHAPTER II

A CRITICAL REVIEW OF LITERATURE

Flow over bottom-rack belongs to the category of spatially varied flow with decreasing discharge. Determination of the performance of a bottom-rack is a complex problem involving a large number of variables. Many investigations have been carried out with a view to evolve a proper design for a bottom-intake. Serious efforts to analyse and understand the phenomenon of flow over bottom-racks, however, have been devoted only since last three decades. Some of the important works are reviewed below:

2.1 Longitudinal Bar Bottom-Racks:

A retional approach to the problem of bottomracks was given by Mostkow(3). His experiments were conducted
on intakes having longitudinal bar bottom-racks. For the analysis, he assumed that for such bottom-racks the specific energy
of the flow all over the rack remains constant and is taken as
effective head causing the flow through the rack. The discharge per unit length of rack, by considering it as an orifice,
was given as

$$\left(-\frac{dQ}{dx}\right) = C_1 \in B \sqrt{2gE} \tag{2.1}$$

where C_1 = coefficient of discharge of longitudinal bar bottom-racks and E = constant specific energy all over rack.

The differential equation of SVF for horizontal frictionless channel will be

$$\frac{dy}{dx} = \frac{Qy(-\frac{dQ}{dx})}{gB^2y^3-Q^2}$$
 (2.2)

Further, the discharge Q at any section is given by

$$Q = By \sqrt{2g(E-y)}$$
 (2.3)

substituting Eqs. (2.1) and (2.3) in (2.2) and integrating the final equation hence found, a equation for water surface profile was obtained as:

$$X = \frac{E}{C_{1}E} \left(\frac{y_{1e}}{E} \sqrt{1 - \frac{y_{1e}}{E}} - \frac{y}{E} \sqrt{1 - \frac{y}{E}} \right)$$
 (2.4)

The value of the coefficient C_1 was assumed to be constant for a particular slope of the rack. He suggested that the value of C_1 varies from 0.435, for a grade of 1 on 5, to 0.497, for a horizontal slope of the rack.

Noseda (5) has analytically studied the characteristics of a longitudinal bar bottom-intake. His assumptions are similar to that of Mostkow, with an addition that the approach flow to the rack is critical. The discharge per unit length of the rack was defined as

$$\left(-\frac{dQ}{dx}\right) = C_n \in B \sqrt{2gy} \tag{2.5}$$

where $C_{n}=\text{coefficient}$ of discharge . The critical approach flow was given as

$$Q_S^2 = gB^3 y_{1e}^3 \tag{2.6}$$

The discharge diversion ${\rm Q}_{\rm D}/{\rm Q}_{\rm S}$ from constant specific energy criteria and Eq. (2.6) is

$$\frac{Q_{D}}{Q_{S}} = 1 - \left[2\left(\frac{3}{2} - \frac{y_{2e}}{y_{1e}}\right)\right]^{1/2} \frac{y_{2e}}{y_{1e}}$$
 (2.7)

Eqs. (2.5) and (2.7) were combined and integrated to provide the relationship between two brink depths and length of the rack:

$$\sqrt{2} C_{n} \in L/y_{le} = \frac{3}{4\sqrt{2}} \left(\sin^{-1}(1/3) - \sin^{-1}(\frac{4y_{2e}}{3y_{le}} - 1) + \frac{3}{2} \left(1 - (\frac{3y_{2e}}{y_{le}} - \frac{2y_{2e}^{2}}{y_{le}^{2}})^{-1/2} \right) \tag{2.8}$$

Finally, the general diversion characteristics relating the diverted flow and the stream flow was derived as a plot, using:

$$(\sqrt{2} \ C_n \in L/\gamma_{1e})^{-3/2} = \frac{Q_S/B}{g^{1/2}(\sqrt{2} \in C_n)^{3/2}L^{3/2}}$$
 (2.9)

Naseda suggested that C_n is independent of stream flow Q_{\S} and aspect ratio of the bars (D/L). Assuming C_n as 0.815 for a given rack geometry and y_{le}, y_{2e} with the help of above Eqs. (2.7,2.8,2.9) a design chart as a plot of

$$\frac{Q_{D}/B}{g^{1/2}(\sqrt{2} \in C_{n})^{3/2} L^{3/2}} \text{ Vs } \frac{Q_{S}/B}{g^{1/2}(\sqrt{2} \in C_{n})^{3/2} L^{3/2}} \quad \text{has been}$$

recommended by Noseda to study the diversion characteristics.

White, et al (14) conducted model tests and compared the performance of bottom-intakes having different

length of bars, bar spacing, the transverse slope of the top surface of the bars and analysed the data on the basis of Noseda's work. The tests were conducted on racks made of longitudinal bars with special sloping top surfaces. Racks were kept at a constant longitudinal slope of 1 vertical on 5 horizontal. In these tests the value of € ranged from 0.167 to 0.333 and L/w from 6 to 10 where w= width of rack bars. This study has shown that C_n is not independent of stream flow as suggested by Noseda. A design chart based on the model tests, as a plot of $\frac{Q_S}{BL \in V | QW}$ Vs $\frac{Q_D}{BL \in V | QW}$ valid for 6 $<\frac{I}{w}$ < 10; 0.167<E< 0.333 and critical approach flow to the rack only has beengiven by them. Further, regarding the shape of bars white, et al suggested that a '' no flow rejection' along the top of bars at lower stream flows can be achieved by providing the transverse top surface slope on the bars, having value between 1 in 3 to 1 in 2.

2.2 Transverse Bar Bottom-Racks:

Subramanya and Sengupta (8,10) have conducted an extensive experimental study on the flow over transverse bar bottom-racks. The racks were made of rectangular bars of width w. It was shown that Mostkow's coefficient of discharge C_1 depends upon the approach state of flow, viz whether subcritical or supercritical and on the aspect ratio w/L of bars. When the approach flow is supercritical, C_1 varies significantly with the area factor. The coefficient C_1 decreases as the approach flow Froude number is increased and the influence

of w/L is less pronounced. The same trend appears to exist when the approach flow is subcritical, though w/L has more pronounced effect on the value of C_1 . Further, it was found that value of C_1 is large for subcritical flows than for supercritical flows. They have not studied the effect of inclination of the rack on C_1 . The assumption of constant specific energy through out the rack length, for determination of the water surface profiles, is questionable.

Rangaraju, et al (7) studied the flow over bottom-racks comprising of transverse circular bars. The experimental study was limited to subcritical approach flows only. A set of equations relating the length of the rack to hydraulic parameters and empirical relations for the contraction coefficient as well as the discharge coefficient have been proposed. It has been shown that the coefficient of contraction is mainly the function of Reynolds number of the approach flow, Froude number of the flow over rack and the opening area ratio of the rack. Further, it was shown that there is an energy loss over the rack which ranges from 20 percent to 50 percent of the initial specific energy. A method of computing the discharge through-racks and the depths at the inlet and exit has been proposed.

2.3 Perforate Plate Bottom-Racks:

An analytical and experimental study conducted by Mostkow (3), is perhaps the major work available for perforated plate bottom-racks. For the analysis, he assumed that the effective head causing the flow is equal to the

depth of flow over the rack. The outflow discharge per unit length through the rack, was presented as

$$\left(-\frac{dQ}{dx}\right) = C_2 \in B \sqrt{2gy} \tag{2.10}$$

where C_2 = coefficient of discharge for perforated plate bottom-racks. The differential equation of SVF assuming the channel to be horizontal and frictionless, will be

$$\frac{dy}{dx} = \frac{Qy \left(-\frac{dQ}{dx}\right)}{gB^2y^3 - Q^2}$$
 (2.11)

substituting Eqs (2.16) and (2.3) in Eq. (2.16) and integrating by using the boundary condition $y = y_{le}$ at X = 0, yields the SVF prafile for perforared plate bottom-racks as

$$X = \frac{E}{\in C_2} \left[\frac{1}{2} \left(\cos^{-1} \sqrt{\frac{y}{E}} - \cos^{-1} \sqrt{\frac{y_{1e}}{E}} \right) + \frac{3}{2} \left(\sqrt{\frac{y_{1e}}{E}} \left(1 - \frac{y_{1e}}{E} \right) \right) - \sqrt{\frac{y}{E}} \left(1 - \frac{y}{E} \right) \right]$$
(2.12)

Mostkow (3) found that C_2 is constant for a particular slope of the rack and varies from 0.750, for a grade of 1 on 5, to 0.800, for a horizontal slope of the rack. Sengupta (8) has shown the variation of C_2 with F_1 , \in and w/L for supercritical approach flows. Subramanya (10) suggested that C_2 could be expected to be given by

$$C_2 = \text{fn} (F_1, \in , \lambda_1, \lambda_2)$$
 (2.13)

where λ_1 = a hole spacing parameter and λ_2 = a hole arrangement parameter. No extensive analysis and experimental study is available regarding the variation of C_2 .

2.4 <u>Slots</u>:

Studies on hydraulic characteristics of bottom-slots have been reported by Venkataraman (4,11,13) and Ramamurthy (6). Venkataraman, et al (4) have conducted an analytical and experimental study of the flow with a slot spanning the entire width of the channel. Defining the coefficient of discharge through the slot $C_{\rm dv}$ as:

$$C_{dv} = \frac{Q_{D}}{BL \sqrt{2gE_{1}}}$$
 (2.14)

where $E_{l}=$ specific energy of the flow at inlet. An expression for the variation of $C_{\rm dv}$ has been obtained as

$$C_{dv} = 0.611 \sqrt{1 - (V_1^2/2gE_1)}$$
 (2.15)

The Equation 2.15 was also verified experimentally for subcritical as well supercritical approach flows. A momentum formulation for the brink depth ratio y_{1e}/y_{2e} has been proposed. The ratio Q_D/Q_S is defined as performance factor of the slot and is found to be a function of L/y_c given as:

$$\frac{Q_{\rm D}}{Q_{\rm S}} = 0.59 \, (L/y_{\rm c}) + 0.04 \, (L/y_{\rm c})^2 \qquad (2.16)$$

Venkataraman (11,13) defined another coefficient of discharge $C_{
m dvl}$ as

$$C_{\text{dvl}} = \frac{Q_{\text{D}}}{BL \sqrt{2gy_{1e}}}$$
 (2.17)

and observed experimentally that it is invariant with F_1 and γ_{1e}/L but decreases with the increase in length L of the opening.

Ramamurthy, et al (6) based on two dimensional channel outlet model and experimental data, presented a functional relationship between the discharge coefficient C_{dr} and the velocity parameter η_1 with $\frac{L}{y_{1e}}$ as the group parameter for the floor slot discharge, as

$$C_{\rm dr} = 0.611 + C_{\rm lr} \eta_{\rm l}^2 + C_{\rm 2r} \eta_{\rm l}^4 + C_{\rm 3r} \eta_{\rm l}^6 + \cdots \qquad (2.18)$$
 for $0 < \frac{L}{y_{\rm le}} \le 1.0$; $0 < \eta_{\rm l} \le 1.0$ where $C_{\rm lr} = -0.538 + 0.254$ $(\frac{L}{y_{\rm le}})$; $C_{\rm 2r} = 0.058 + 0.234$ $(\frac{L}{y_{\rm le}})$ and $C_{\rm 3r} = -0.129 - 0.489$ $(\frac{L}{y_{\rm le}})$ (2.19) $\eta_{\rm le} = \frac{1}{1 + \frac{2P_{\rm c}}{F_{\rm l}^2}}$ (2.20)

and P_c = Pressure correction factor for curvilinear flows = fn (L/y_c)

Venkataraman, et al (12) have conducted on experimental study including all types of bottom-racks and slot. They have shown that the assumption of constant specific energy along the rack is confirmed for subcritical approach flows for racks with small openings. In all other cases an energy decrease along the rack was noted, but no detailed study in this regard is reported.

2.5 <u>Conclusions</u>:

On reviewing the available literature it is observed that results of many investigations are of very limited nature. Most of them belong to the category of transverse bar bottom-racks or slots. Further, the assumption of constant specific energy all over the rack is questionable. Since the parallel bar bottom-racks are important from the point of view of practical applications, it was felt worth while to conduct an experimental study for analysing the flow over such racks including as many variable as possible.

CHAPTER III

EXPERIMENTS AND OBSERVATIONS

3.1 Experimental Set-up:

To study the hydraulic behaviour of horizontal longitudinal bar bottom-racks, experiments were carried out in the hydraulic laboratory of the Indian Institute of Technology, Kanpur. The experiments were conducted in two flumes, Flumes A and B, with details as given below:

Table 3.1 Details of Flumes Used in the Experimental Study

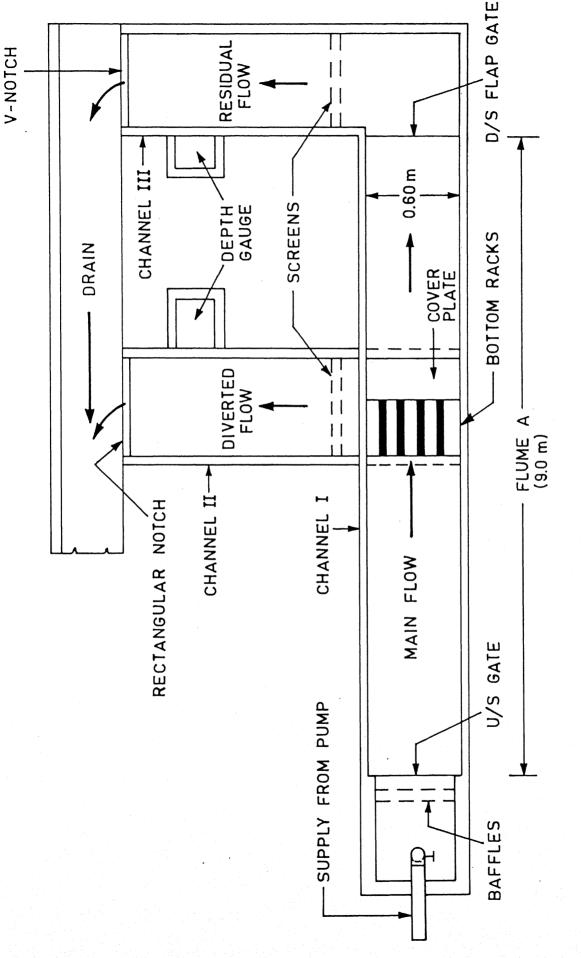
	Flume A	Flume B
Width	0.60 m	0.15 m
Length	9.00 m	3.00 m
Туре	Non-recircula- ting	Partially -recir- culating
Bed	Horizontal and Smooth	Horizontal and Smooth
Side Walls	Masonry Side Walls	Plexi-glas Side Walls
Cross-Section	Rectangular	Rectangular
Max.Discharge Available	95 Liters/S	18 Liters/S
Upstream Contro	1 Sluice Gate	Sluice Gate
Downstream Control	Bottom-hinged Flap Gate	Sluice Gate

The diverted flow through the rack in flume A was passed through channel No. II and measured by a rectangular-notch fitted at it's down stream end. Residual flow was passed

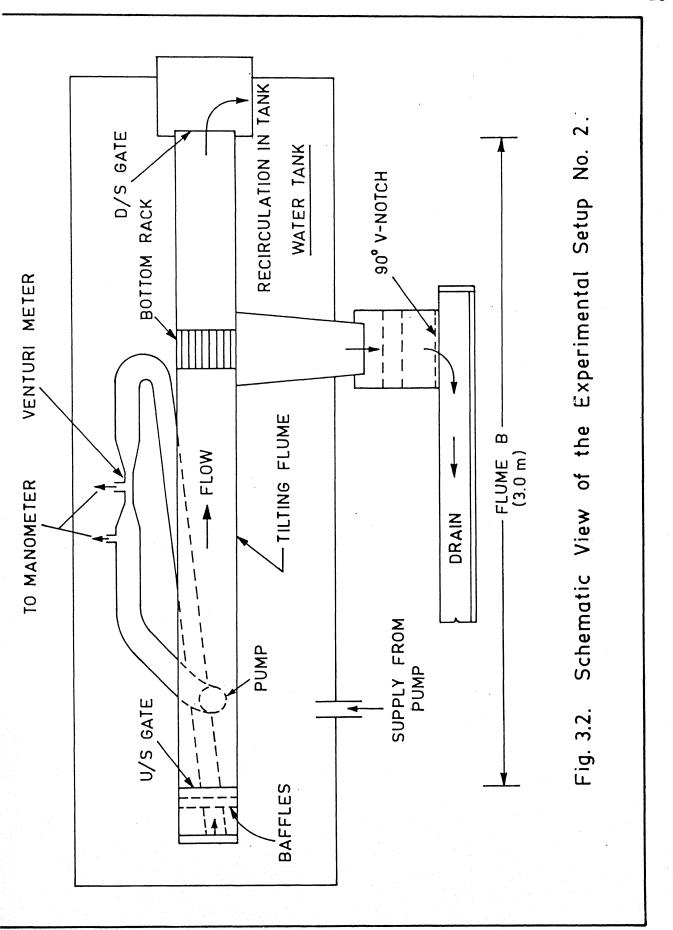
through channel No. III and measured by a V-Notch. The Notches were calibrated before starting the experiments. A schematic view of experimenal set up No. 1 for flume A is given in Fig. 3.1 The diverted flow through the rack in flume B was measured by a 90° V-Notch and the total stream flow was measured by a calibrated vinturimeter fitted in the supply pipe. For the head measurements in Notches, point guages with least count of 0.1 mm were used. A schematic view of experimental set up No.2 for flume B is given in Fig. 3.2.

In flume A, a slot having width B = 60 cm and Lenth L= 30 cm, was cut at a distance of 5 meter, from the upstream gate. The rack made of circular bars could be placed in this slot. The diameter D of the bars was kept 22 mm and the bars were placed at uniform clear spacing S. Keeping D = 22 mm as constant and varying the spacing S, four sets of racks were prepared having D/S ratios of 1.13, 2.05, 2.90 and 5.60. Then for the same rack by using a cover plate beneath and filling the gaps by cement mortar uniformly, the length of the rack was reduced to 15 cm, to achieve B/L=4.0. All the four rack sets having the D/S ratios mentioned above were also tested by making B/L = 4.0. With the available discharge and downstream control only supercritical approach flow could be obtained in flume A.

In flume B, a slot of width B=1.5 cm and length L=7.5 cm. was cut at a distance 2.56 meters, from the



Schematic View of the Experimental Setup No. 1. Fig. 3.1.



upstream gate. Circular bars of diameter 6 mm were used for all the rack assemblies and the bars were placed at uniform clear spacing. The spacing S was changed for different rack sets to achieve four sets of D/S ratios of 1.17, 1.89,3.33 and 5.50. With the help of small angles placed underneath the rack from both sides, the length could be reduced to 3.75 cm to achieve B/L = 4.0 for all the four rack sets. With the available discharge and downstream control only subcritical approach flow could be obtained in this flume. For the study of flow over a pure slot the flume B was chosen and a slot having B=15 cm was made. After this study, the slot length was reduced to 3.75 cm to get B/L = 4.0. When the whole flow was diverted within certain length of rack, this particular length was taken as L.

Table 3.2 Range of Parameters in the Experimental Study

Parameter	Range
D/S	1.13 to 5.60
ϵ	0.157 to 0.487
B/L	2.00 and 4.00
${f D}$	0.60 cm and 2.20 cm
Fo	0.200 to 5.40
R _{er}	$3.5 \times 10^3 $ to 3.5×10^4
R _{eo}	$1x10^4$ to $1.95x10^5$
$V_0^2/2gE_0$	0.02 to 0.95

3.2 Range of Parameters:

A total of 146 runs were conducted and the range of various parameters studied are shown in Table 3.2.

Where
$$F_0 = \frac{V_0}{\sqrt{g} y_0} = \text{froude number of approach flow at section (0) defined in Fig. 1.1.}$$

$$R_{eo}$$
 = Approach flow Reynolds number at section (0) = $\frac{Q_S}{RV}$

$$R_{er} = \frac{\frac{Q_S}{BV}}{\frac{Q_D \times D}{BL \in \mathcal{D}}} = \text{Reynolds number of the flow through}$$
the rack.

 \mathcal{V} = Kinematic viscosity of water; and

QD = Diverted flow through the rack.

The present study fairly covers the usual practical ranges of parameters used in the design of Trench weirs, as can be seen from Table 3.3 where some parameters corresponding to the design data of trench weirs are given.

3.3 Observations:

For a given rack in a flume, a series of experiments were conducted starting from the smallest discharge and gradually increasing it in steps till the maximum discharge capacity of the flume was reached. In a typical experiment the centre line depth of flow along the flume at different sections were measured with a movable point guage of least count 0.1 mm. On the basis of the water surface profiles that exist over the rack and the approach flow, the flows can be grossly classified into two categories viz, subcritical and supercritical approach flows.

Table 3.3 Range of Parameters of Some Trench Weir Installations

Parameters	Binwa Hyde Banu Weir	l Project(9 0) Parai Weir	Andhra Hydel Project (2)
D/S	0.8333	0.8333	1.333
\in	0.490	0.490	0.429
B/L	7.000	3.000	26.670
D	2.5 cm	2.5 cm	4.0 cm
Fo	2,00	1.10	_*
Rer	5.6x10 ³	2.0x10 ⁴	1.4x10 ⁴
$V_0^2/2gE_0$	0.670	0.370	_{Eus} *

^{* =} Data not available

3.3.1 Subcritical Approach Flow:

In the case of subcritical approach flow the depth of flow continuously decreases from upstream gate to the beginning of the rack. It is observed that the flow becomes supercritical at the inlet to the rack, hence producing a critical flow condition a little distance upstream from the inlet. The depth of flow decreases along the rack and super critical flow exists all over it. Downstream of the rack the depth increases slightly due to friction. Depending upon the tail water condition a jump may occur downstream to the rack. This jump may shift upstream and may form even in the middle of the rack itself. So long as the inlet

depth y_{le} is not affected by the jump (i.e. tail water) such flows are designated as 'Free flows'. When the jump shifts further upstream the inlet becomes submerjed and the flow becomes subcritical all along the channel. Thus, three types of flows could be identified in this category:

Al : Subcritical approach flow and super critical flow all over the rack. This is called 'subcritical approach free flow.'

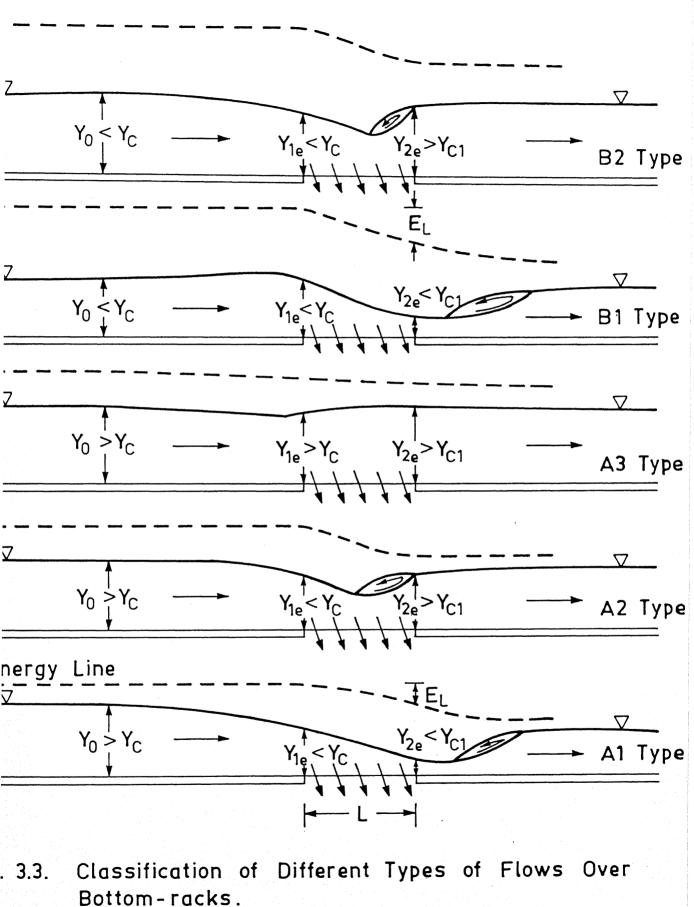
A2 : Subcritical approach and partial supercritical over the rack.

A3 : Subcritical flow all along the channel. This is called 'Subcritical approach submerged flow'.

All the three types of flows are shown in Fig. 3.3. In this figure $y_{\rm c}$ is upstream critical depth and $y_{\rm cl}$ stands for downstream critical depth.

3.3.2 Super Critical Approach Flows:

In the category of supercritical approach flows it was observed that for lower Froude numbers (say $F_0=1.2$) the water surface drops from the upstream gate to the beginning of the rack. The depth of flow decreases along the rack and the flow along it will also be supercritical. After the end of the rack the depth increases slightly due to friction. The same trend is observed for all the lower Froude numbers ($R_0=1.0$ to 1.4). But when the Froude number is more than about 2.0 the depth increases from upstream gate upto about



the beginning of the rack due to high channel friction and drops down at the beginning of the rack. Depending upon the downstream control, a jump may some time occur downstream of the rack and may shift upstream to produce subcritical flow in the neighbourhood of inlet in the approach channel. Also it can be observed that for Froude numbers greater than 2.0 there is lesser difference between y_{2e} and y_{1e} compared to that in the Froude number range of 1.0 to 1.4. Thus two types of flows may be clearly identified:

- Bl : Supercritical approach flow and supercritical flow all over the rack.
- B2 : Super critical approach flow and partial subcritical over the rack.

Bl and B2 types of flows are shown in Fig. 3.3. Typical observed water surface profiles for different types of flows A1,A2 and A3 are shown in Fig. 3.4. Fig. 3.5 shows the profiles, all corresponding to B1 flows only. For a few runs the velocity profiles were also measured at certain sections of the channel. Some of the observed velocity profiles are shown in Fig. 3.6.

The present investigation is confined to the study of Al,A3 and Bl flows. The flow types A2 and B2 are beyond the scope of the present study in view of the complex flow situations. The data collected in Al, A3 and Bl flows are summarised in Appendix I.

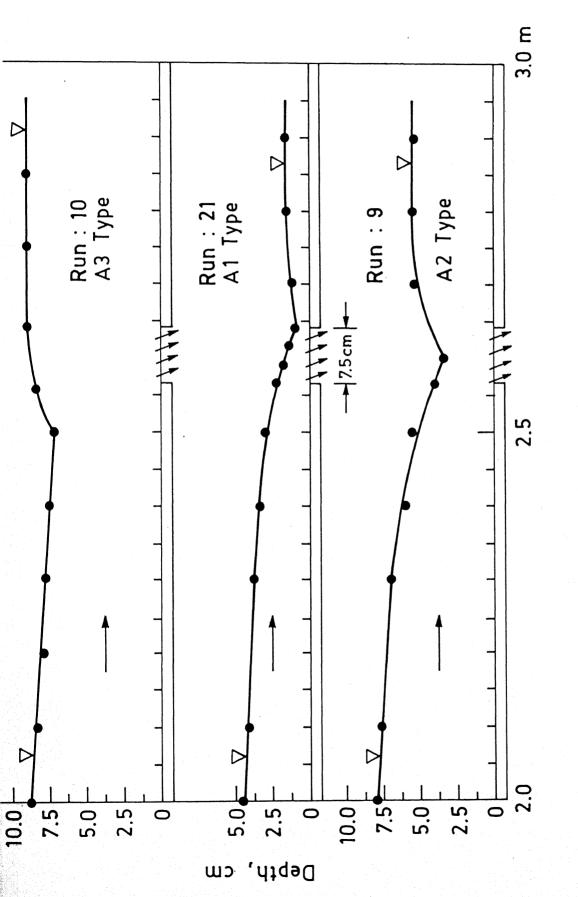
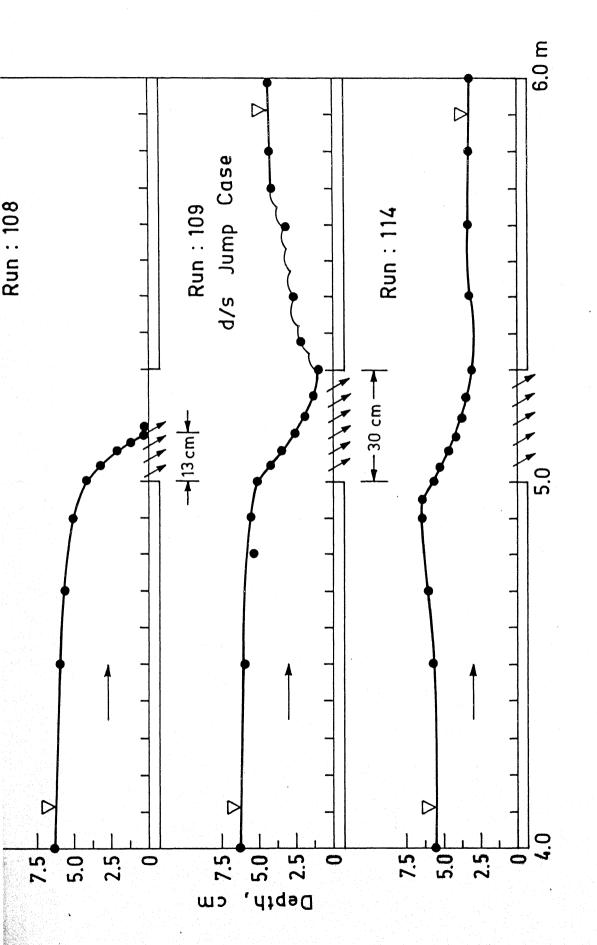
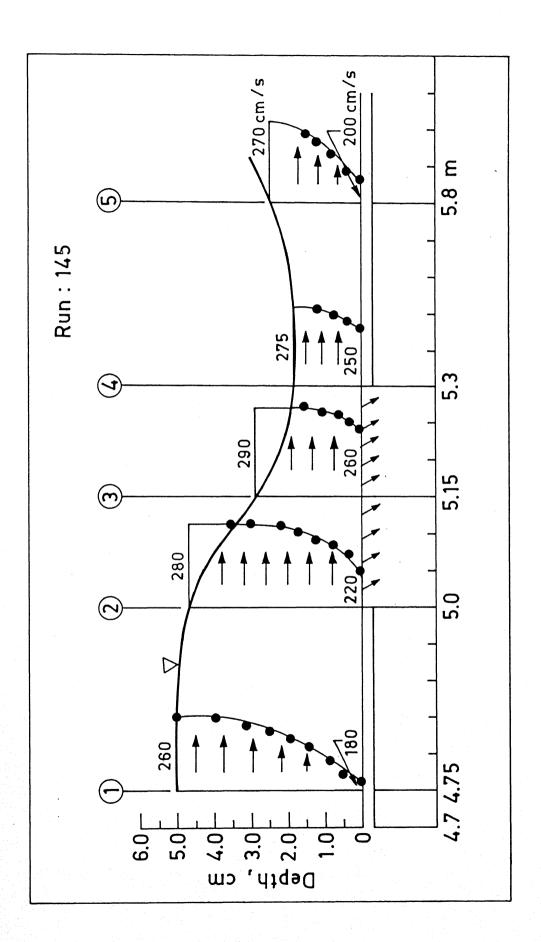


Fig. 3.4. Typical Water Surface Profiles in Subcritical Approach Flows.



Typical Water Surface Profiles for Super-critical Approach Flows (B1 Type). Fig. 3.5.



Observed Typical Velocity Profiles. Fig. 3.6.

CHAPTER IV

ANALYSIS

4.1 Study of The Limiting Inlet Depth:

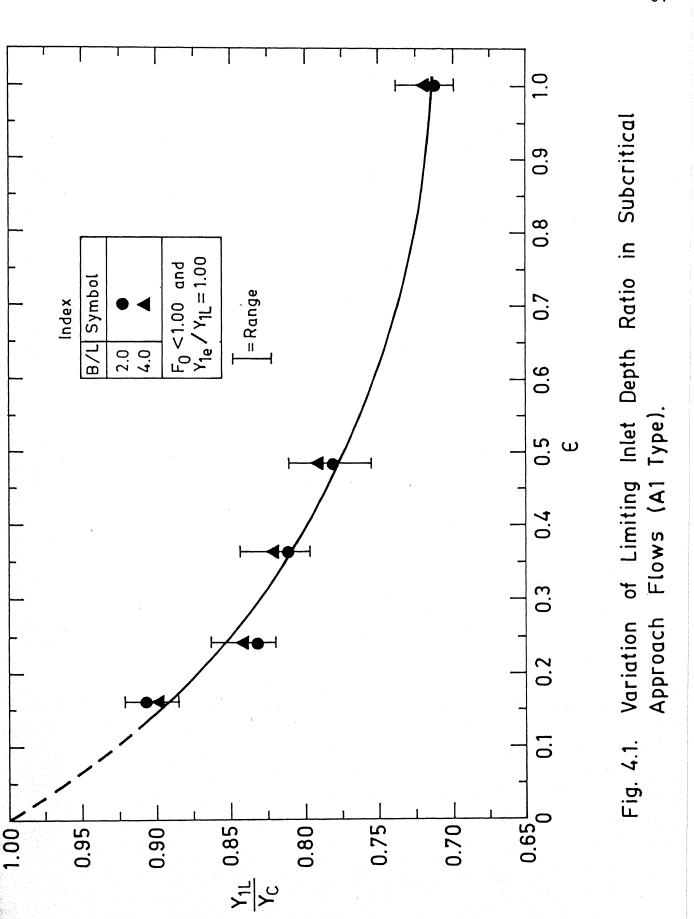
4.1.1 Subcritical Approach Flows:

As indicated earlier in section 3.3.1 and shown in Fig. 3.3, three types of flows (viz, Al,A2,A3) are possible for subcritical approach flow case. The limiting inlet depth y_{lL} is introduced with a view to differentiate the free and submerged flows. For Al and A2 types of flows the inlet depth $y_{le}=y_{lL}$ and for A3 type of flow the inlet depth $y_{le}>y_{lL}$. In a subcritical flow with a sudden drop, the depth y_{lL} will be the end depth. For rectangular channels, subcritical flows it's value will be a constant at 0.715 y_c . Also for any channel shape, in subcritical flows, the end depth ratio y_{lL}/y_c is independent of the Froude number (10). Hence, for Al type flows over longitudinal bar bottom-racks, the ratio y_{lL}/y_c can be represented as

$$\frac{Y_{1L}}{Y_{C}} = fn (B/L, \in)$$
 (4.1)

Fig. 4.1 shows the variation of the limiting inlet depth ratio $\frac{y_{1L}}{y_c}$ with \in for B/L = 2.0 and 4.0. It is seen that

 $\frac{y_{1L}}{y_c}$ decreases with ϵ and is unaffected by the value of B/L . A best fit equation for the variation of the limiting



inlet depth ratio was obtained as

$$\frac{y_{1L}}{y_{c}} = -0.215 \text{ Log} \in +0.715$$
 (4.2)

Eq. (4.2) is useful in determining the existence of A3 type flows.

4.1.2 Supercritical Approach Flows:

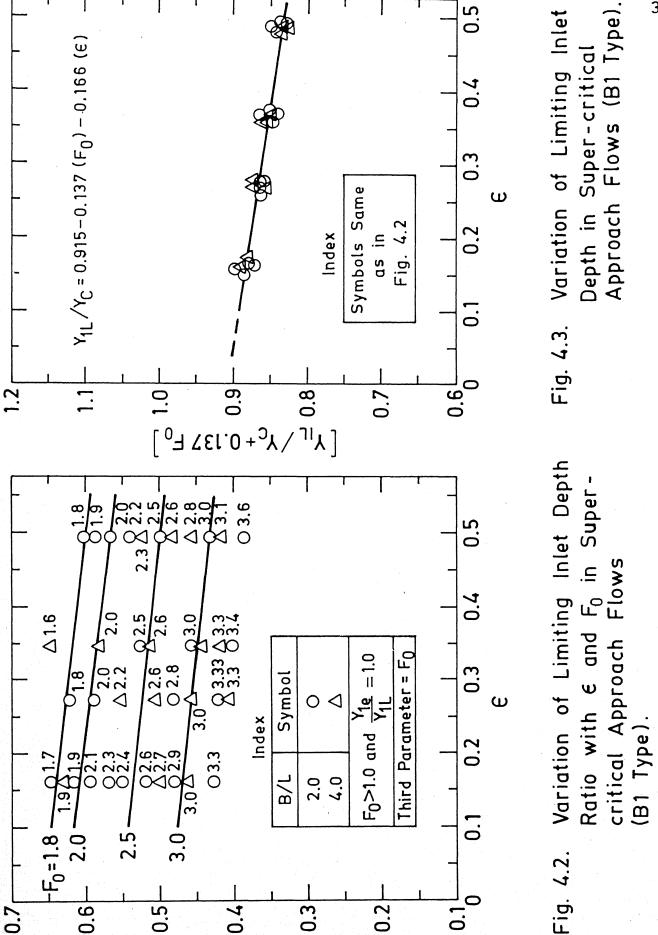
As indicated in section 3.3.2, in supercritical approach flows two types of flows over the rack are possible and these viz Bl and B2 type flows, are shown in Fig.3.3. From an analogy of end depths at sudden drops in supercritical flows, for Bl and B2 types of flows over racks $\frac{y_{1L}}{y_c}$ can be expected to be a function of Froude number also and can be represented as

$$\frac{y_{1L}}{y_{c}} = \text{fn } (B/L, \in , F_{0})$$
 (4.3)

Fig. 4.3 shows the variation of $\frac{y_{1L}}{y_c}$ with \in and B/L, by taking F_o as a third parameter. It is seen that the B/L does not have any effect on $\frac{y_{1L}}{y_c}$. The effect of F_o on $\frac{y_{1L}}{y_c}$ for a given \in was found to be related by a linear relationship and the relation between the three parameters found by the best fit technique is:

$$\frac{y_{1L}}{y_{c}} = 0.915 - 0.137 F_{o} - 0.166 \in (4.4)$$

Fig. 4.4 shows the validity of Eq. (4.4). The correlation is very good and as such this Equation can be used with



confidence for predicting y_{lL} in supercritical approach flows over longitudinal bar bottom-racks.

4.2 Study of The Coefficient of Discharge C_d:

4.2.1 Parameters:

The pressure distribution at the inlet of the rack will in general be different from the hydrostatic pressure distribution—due to the curvature of the flow. In the extreme case of a sudden drop (and also a slot) it is known that the critical depth y_c occurs at about $5y_e$ and at that section the flow is essentially parallel and the hydrostatic pressure distribution exists there. As such a section at a distance of 5 y_{1e} upstream from the inlet was chosen for defining the approach flow parameters. At this section the specific energy E_o was taken as $E_o = y_o + \frac{V_o^2}{2g}$. Assuming an orifice type flow through the rack with an operating head equal to the energy head E_o over the entire rack, a coefficient of discharge C_d through the longitudinal bar bottomaracks is defined as

$$C_{d} = \frac{Q_{D}}{BL \in \sqrt{2gE_{0}}}$$
 (4.5)

where Q_D = diverted flow through rack. The possible variables influencing C_d may be grouped as:

$$C_d = fn(V_o, y_o, B, L, D, S, g,), longitudinal slope$$
(4.6)

Hence the dimensionless groups of variables will be

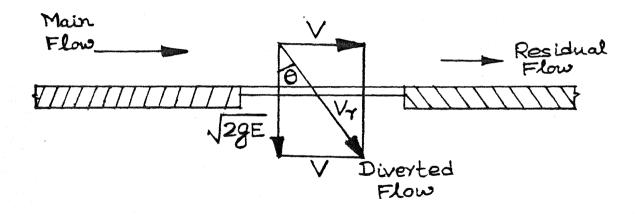
$$C_{d} = \text{fn} \left(\frac{V_{o}}{\sqrt{gy_{o}}}, \frac{V_{o}y_{o}}{V}, \frac{B}{y_{o}}, \frac{B}{L}, \frac{D}{S}, \frac{D}{B}, \text{longidutinal} \right)$$

For horizontal bottom-racks, longidudinal slope =0 and for two dimensional flow cases $\frac{B}{y_0}$ may be considered to be an insignificant parameter. Out of the two rack parameters D/S is considered to be significant and the other viz, D/B can be considered to be insignificant especially for very low values of D/B. For turbulent flows $\frac{V_0 y_0}{V}$ = Reynolds number of the approach flow being very high may be considered to have negligible effect over C_d . Hence for analysis in the practical ranges, the functional variation of C_d is taken as

$$C_d = fn \left[F_o, \frac{D}{S}, \frac{B}{L} \right]$$
 (4.8)

If V = mean flow velocity in the channel, the resultant velocity V_r is given by $V_r = \sqrt{V^2 + 2gE}$ as shown in Fig.A4.O5. The velocity through the rack, when assumed as an orifice flow, is directly proportional to $\sqrt{2gE}$, where E is the specific energy at any section over the rack. Also the parameter $\frac{V^2}{2gE} = \tan^2\theta$ where θ = angle of inclination of the resultant velocity V_r with the vertical. Hence greater the angle θ lesser will be the effective area carrying the diverted flow, Hence lesser will be C_d . Thus $\frac{V^2}{2gE}$ seem to be an important parameter affecting the C_d . This parameter can be represented as

$$\frac{V^2}{2gE} = \frac{V^2}{(2gy+V^2)} = \frac{1}{(1+2/F^2)}$$
 (4.9)



ig. A 4.05

Velocity Triangle of the Flow Diverting Through the Rack.

where F= Froude number of the flow at any section. For the purpose of analysis, the dimensionless parameter $\frac{V_0^2}{2gE_0}$ can be taken to be representative of $\frac{V_0^2}{2gE}$ for given rack and inlet conditions. In view of this, the parameter $\frac{V_0^2}{2gE_0}$ is used in the place F_0 in Eq (4.8) to represent C_d as

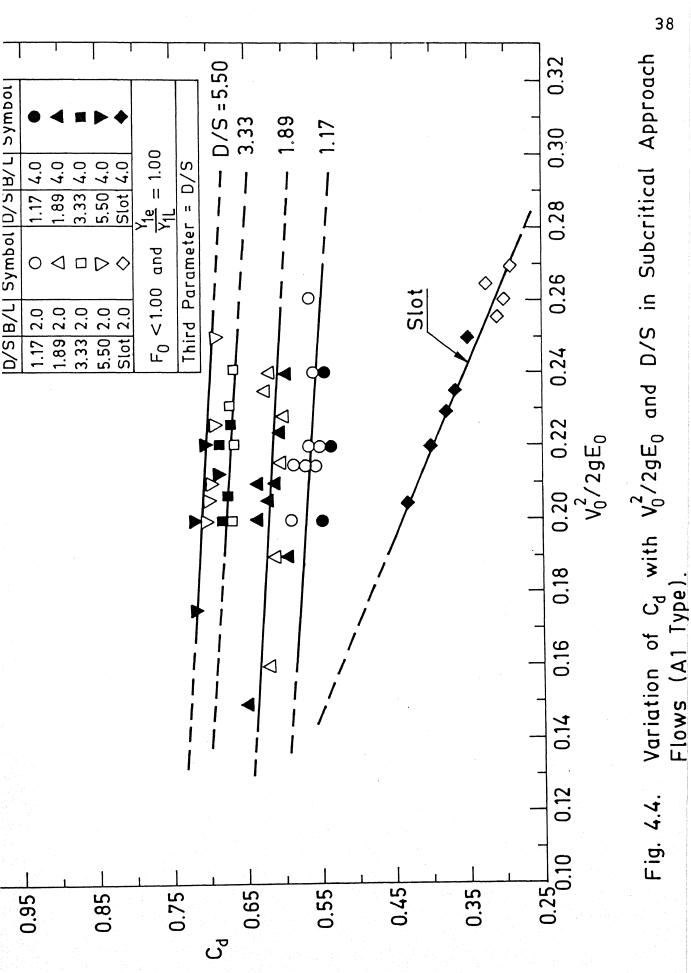
$$C_{d} = fn \left(\frac{V_{o}^{2}}{2gE_{o}}, \frac{D}{S}, \frac{B}{L} \right)$$
 (4.10)

It may be mentioned that a parameter similar to $\frac{\sqrt{2}}{2gE_0}$ has also been used previously by Venkataraman, et al (4) and Ramamurthy, et al (6) to represent the approach velocity effect over the discharge coefficient through bottom-intakes. The term $\frac{\sqrt{2}}{2gE}$ can be called as the Flow parameter for the rack. The parameter D/S is a measure of transverse contraction of the flow for a given opening area ratio. The parameter B/L is a measure of the two dimensionality of flow over the rack representing the possible effects of side walls.

The variation of $C_{\mbox{d}}$ with the parameters given in Eq.(4.10) is analysed separately for Al,A3 and Bl types of flow.

4.2.2 C_d in Al Flows:

For Al flows the variation of C_d with $\frac{V_0^2}{2gE_0}$ by taking D/S as the third parameter is shown in Fig. 4.4. Four values of D/S in each of the two sets B/L =2.0 and 4.0 respectively are plotted in this Figure. Also plotted are the results of experiments of flow over a slot. It is seen



that for a given D/S, there is no effect of B/L and the value of C_d decreases very slowly with $\frac{\sqrt{o}}{2gE_0}$. The trend is consistent for all four values of D/S tested. The variation of C_d for a slot is appropriately located at low values of D/S. However, for a slot, the effect of $\frac{o}{2gE_0}$ is more pronounced, possibly due to the different nature of flow.

The variation of C_d for a given $\frac{V_0^2}{2gE_a}$ was found to be related by a logarithmic relation as

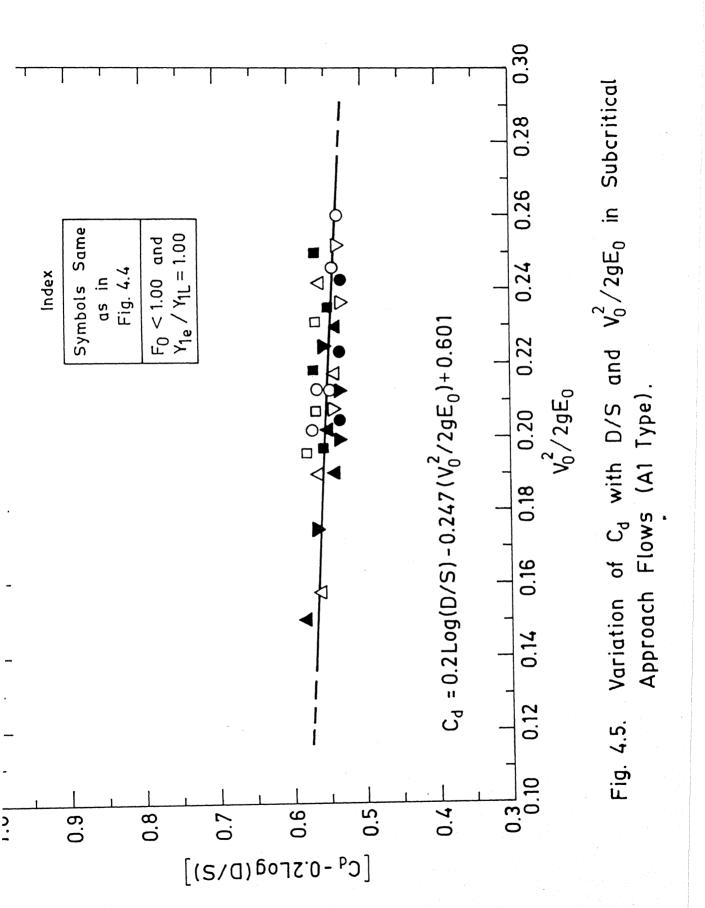
$$C_d = 0.2 \text{ Log } (D/S) + 0.56$$
 (4.11)

within the range of D/S values tested (viz, D/S= 1.17 to The best fit relation for the experimental data on Al flows was obtained as

$$C_d = 0.2 \text{ Log } (D/S)-0.247 \left(\frac{V_o^2}{2gE_o}\right) + 0.601 (4.12)$$

This is shown in Fig. 4.5 where [C_d -0.2 Log (D/S)] is plotted v^2 against $\frac{v_0}{2gE_0}$ and all the data on Al flows are plotted, Eq. (4.12) is also shown in this Fig. It is interesting to observe the small scatters of data and hence the good correlation. As such, Eq. (4.12) can be taken to adequately represent the variation of C_d in Al flows for longitudinal bar bottom-racks. It may be noted that $\frac{V_0^2}{2gE_0}$ has a very small effect on C_d in Al flows, as the term $\frac{V_0^2}{2gE_0}$ will be within

value of 0.33. Hence, the second term in Eq. (4.12) can be neglected within 5 percent error.



4.2.3 C_d in A3 Flows:

For A3 flows C_d can be expected to be given by V_d^2 $C_d=\text{fn}\left[\frac{o}{2gE_0}, D/S, S_b \text{ and } B/L\right)$ (4.13)

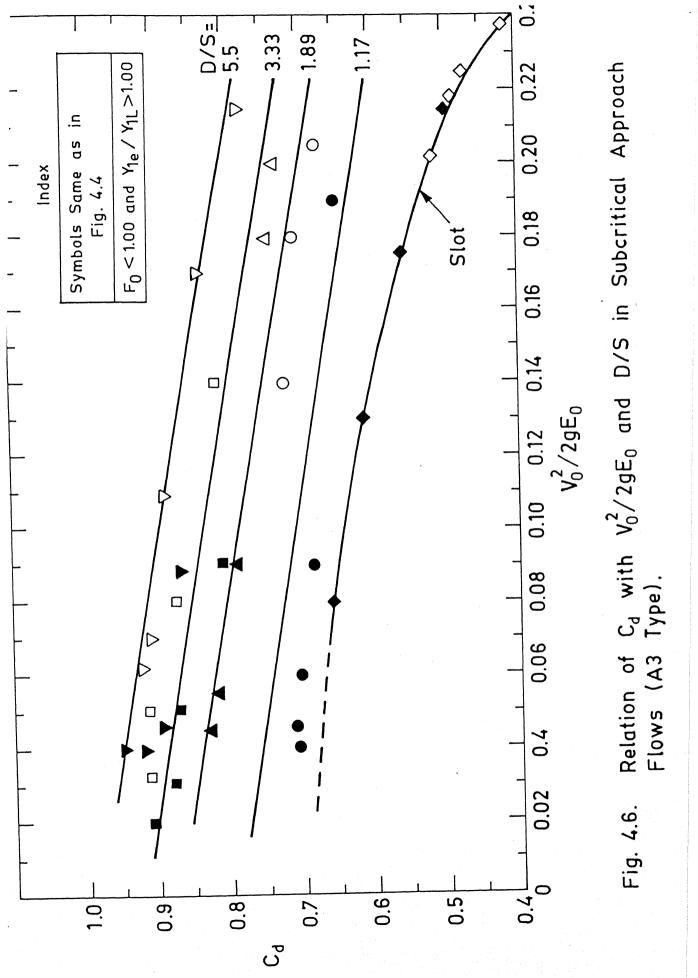
where S_b = submergence of the inlet = $\frac{V_1e^-V_1L}{V_1e}$. For A3 flows the variation of C_d with $\frac{V_0^2}{2gE_0}$ by taking D/S as third parameter is shown in Fig. 4.6. Four values of D/S in each of the two sets B/L = 2.0 and 4.0 respectively are plotted in this figure, the data covers a range of submergence S_b = 0.1 to 0.55. Also plotted are the results of experiments of flow over a slot. It is seen that for a given D/S, there is no effect of B/L and the value of C_d decreases with $\frac{V_0^2}{2gE_0}$. The trend is consistent for all four values of D/S tested. The variation of C_d for a slot is properly located at low values of D/S. Also there was no trend of variation of C_d with S_b . The variation of C_d for a constant $\frac{V_0^2}{2gE_0}$ was found to be related by a logarithmic relation as

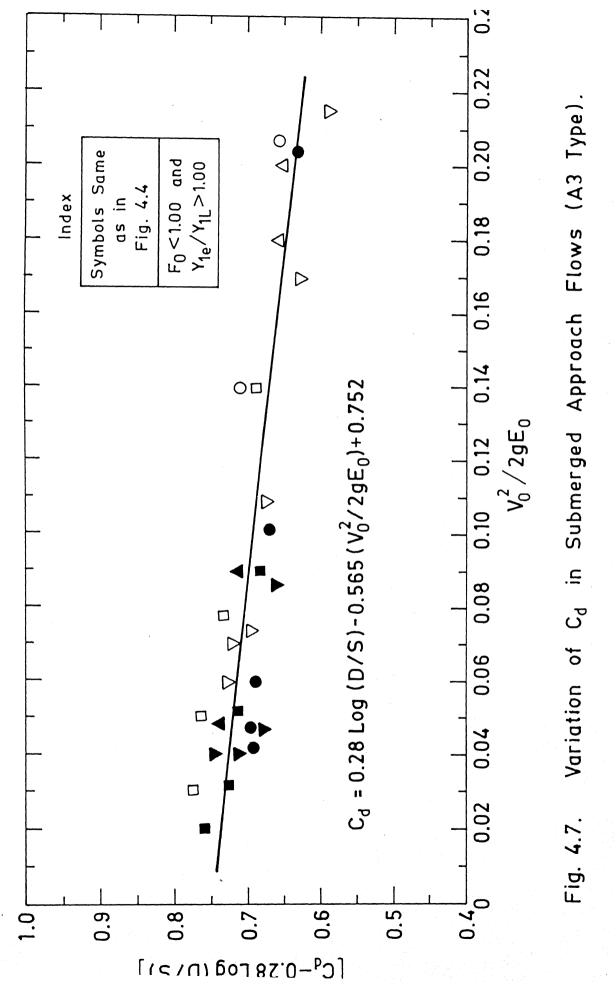
$$C_d = 0.28 \text{ Log } (D/S) + 0.57$$
 (4.14)

within the range of D/S values tested (viz, D/S =1.17 to 5.50). The best fit relation for the experimental data on A3 flows was obtained as

$$C_d = 0.28 \text{ Log}(D/S) - 0.565(\frac{V_o^2}{2gE_o}) + 0.752$$
 (4.15)

This is shown in Fig. 4.7 where $[C_d-0.28 \text{ Log } (D/S)]$ is plotted against $\frac{V_0^2}{2gE_0}$ and all the data on A3 flows are plotted. Eq.(4.15) is also shown. The maximum scatter of experimental





data was found to be \pm 6%. Hence, being a satisfactory correlation Eq. (4.15) can be taken to adequately represent the variation of C_d in A3 flows over longitudinal bar bottom-racks for submergence factor $S_b \leq 0.55$. It may be noted that, compared to Al flows the values of C_d are higher in A3 flows. It is possible that at C_d is a weak function of S_b and at higher submergences Eq.(4.15) may have different coefficients.

4.2.4 C_d in Bl flows:

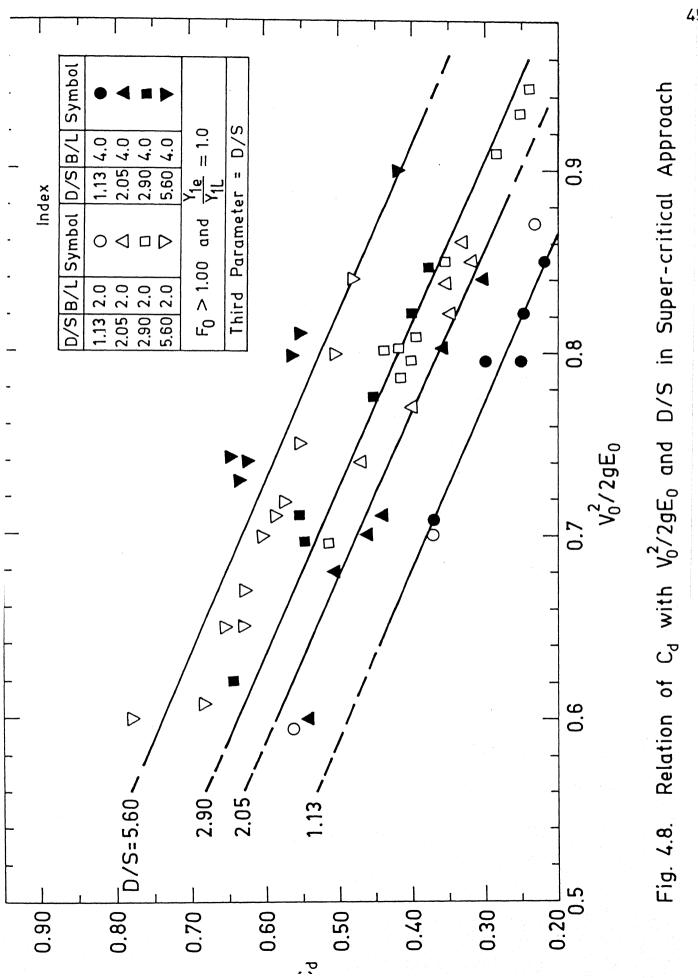
For BI flows the variation of C_d with $\frac{V_o^2}{2gE_o}$ by taking D/S as third parameter is shown in Fig. 4.8. Four values of D/S in each of the two sets B/L = 2.0 and 4.0 respectively are plotted in this figure. It is seen that for a given D/S, there is no effect of B/L and the value of C_d decreases with $\frac{V_o^2}{2gE_o}$. The trend is consistent for all the four values of D/S tested. The variation of C_d for a constant $\frac{V_o^2}{2gE_o}$ was found to be related by a logarithmic relation as

$$C_d = 0.36 \text{ Log (D/S)} + 0.29$$
 (4.16)

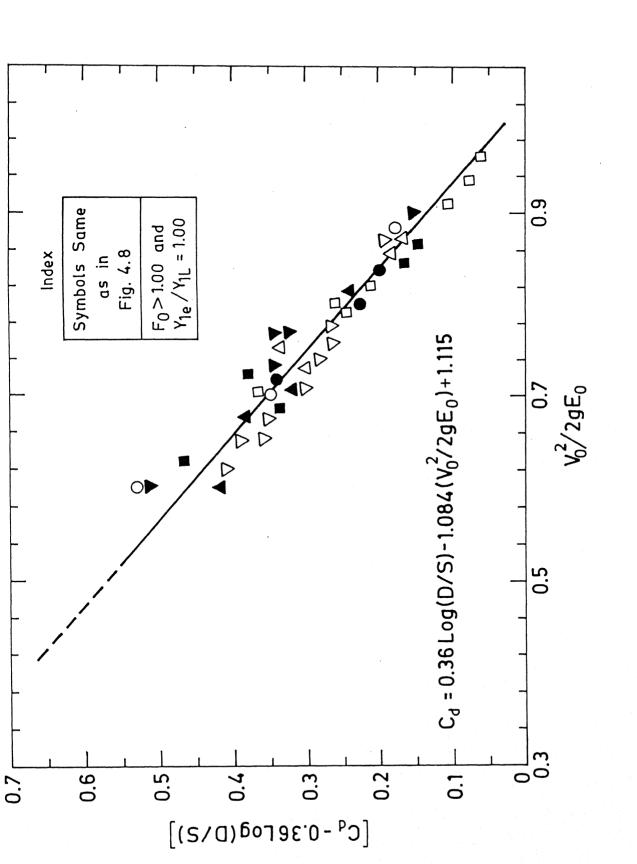
within the range of D/S values tested (viz, D/S = 1.13 to 5.60). The best fit relation for the experimental data on Bl flows was obtained as

$$C_d = 0.36 \text{ Log (D/S)-1.084 (} \frac{V_o^2}{2gE_o}) + 1.115$$
 (4.17)

This is shown in Fig. 4.9 where [C_d -0.36 Log (D/S)] is plotted against $\frac{V_0^2}{2gE_0}$ and all the data on Bl flows are plotted. Eq.(4.17) is also shown in this Fig. The maximum scatter







of experimental data was found to be \pm 10% with an average scatter of 3%, Hence, being a satisfactory correlation Eq. (4.17) can be taken to adequately represent the variation of C_d in Bl flows over longitudinal bar bottom-racks. It is noted that C_d values are affected considerably by the flow parameter $V_0^2/2gE_0$. For a given D/S ratio, C_d values rapidly decrease with increase in $V_0^2/2gE_0$ i.e. with the increase in Froude number of the approach flow.

4.3 Prediction of the Diversion Ratio:

4.3.1 Parameters

While the diverted flow Q_D for a given rack and flow condition can be calculated by using C_d , it is useful for design purposes to directly correlate the diversion ratio to the rack and flow parameters. The diversion ratio of a bottom-rack is defined as the ratio of flow diverted through the rack Q_D to the total stream flow Q_S i.e. Q_D/Q_S . The pertinent variables influencing the Q_D through a horizontal longitudinal bottom-rack may be grouped as

$$Q_D = \text{fn} [Q_S, y_0, \mathcal{Y}, g, B, L, D S]$$
 (4.18) Hence, the dimensionless parameters affecting $\frac{Q_D}{Q_S}$ can be written as

$$\frac{Q_{D}}{Q_{S}} = \operatorname{fn}\left[\frac{L^{3}B^{2}q}{Q_{S}^{2}}, \frac{Q_{S}}{B\nu}, \frac{D}{S}, \frac{D}{B}, \frac{B}{L}, \frac{B}{y_{o}}\right]$$
(4.19)

The dimensionless parameters in simplified form can be rewritten as

$$\frac{Q_{D}}{Q_{S}} = \text{fn} \left[\frac{L}{Y_{C}}, R_{eo}, \frac{D}{S}, \frac{B}{L}, \frac{D}{B}, \frac{B}{Y_{O}} \right]$$
 (4.20)

where R_{eo} = Reynolds number of approach flow

 $y_c = upstream critical depth.$

For turbulent flows, R_{eo} , being very high, may be considered to have negligible influence on the gross characteristics of the phenomenon. Out of the two rack parameters D/S is considered to be significant and the other viz, D/B is considered not significant at very small values. Further by assuming the effect of aspect ratio $\frac{B}{Y_{o}}$ to be insignificant in 2D flows, the diversion ratio is expressed as

$$\frac{Q_{D}}{Q_{S}} = \operatorname{fn}\left[\frac{L}{Y_{C}}, \frac{D}{S}, \frac{B}{L}\right] \tag{4.21}$$

The parameter $\frac{L}{\gamma_c}$ is a measure of the nature of approach flow and the size of the rack. It can be expected that the diversion ratio will increase with $\frac{L}{\gamma_c}$. The parameter D/S is a measure of transverse contraction of the flow for a given opening area ratio . The parameter B/L is a measure of the two dimensionality of the flow over the rack representing the possible effects of side walls. It may be mentioned that the parameter $\frac{L}{\gamma_c}$ has been used by Venkataraman, et al (4) for representing the variation of diversion ratio of a slot.

The variation of the diversion ratio with the parameters as in Eq. (4.21) is analysed separately for Al and Bl flows.

4.3.2
$$\frac{Q_D}{Q_S}$$
 in Al Flows

For AAl flows the variation of $\frac{Q_D}{Q_S}$ with $\frac{L}{\gamma_C}$ by taking D/S as third parameter is shown in Fig. 4.10. Four values of D/S in each of the two sets B/L =2.0 and 4.0 respectively are plotted in this figure. The value of $\frac{B}{\gamma_O}$ in all the data was in the range 1.3-5.8. It can be observed that $\frac{Q_D}{Q_S}$ is not affected by B/L for a given D/S and increases linearly with $\frac{L}{\gamma_C}$. Also, there is no specific effect of B/ γ_O . The trend is consistent for all the four D/S values tested. It is observed that the curve drawn through the experimental points passed through the origin in all the four cases of D/S. This is consistent with the boundary condition Q_D =0 when L=0 i.e., when there is no opening, there is no flow diversion. For a constant D/S, the diversion ratio can be expressed as

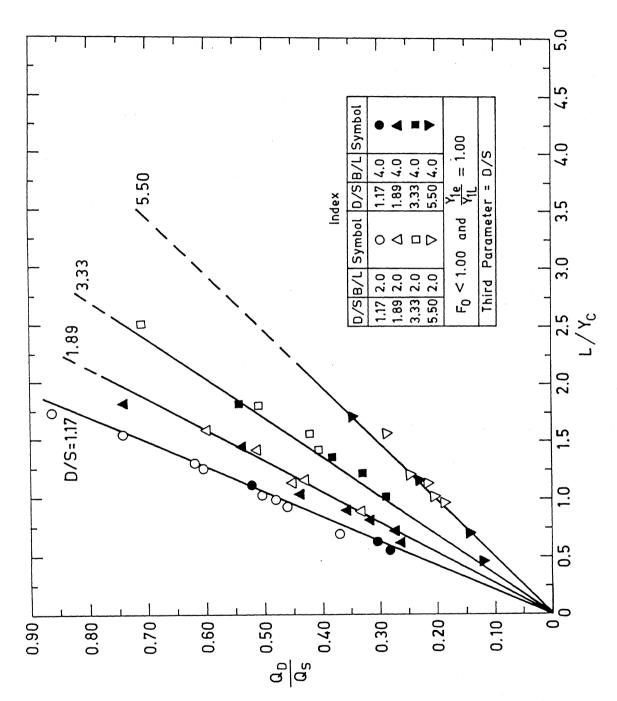
$$\frac{Q_{D}}{Q_{S}} = m_{1} (L/\gamma_{c}) \qquad (4.23)$$

The slope m_1 is a function of D/S as seen in Fig. 4.10. The variation of m_1^* with D/S for Al flows is shown in Fig. 4.12 , from which m_1 can be expressed as

$$m_1 = 0.51-0.41 \text{ Log } (D/S)$$
 (4.24)

Combining Eqs. (4.23) and (4.24)

$$\frac{Q_D}{Q_S} = [0.51 - 0.41 \text{ Log } (D/S)] \frac{L}{Y_C}$$
 (4.25)



Variation of Diversion Ratio in Subcritical Approach Flows (A1 Type). Fig. 4.10.

The minimum length of rack to divert all the incoming flow, $L_{m} \quad \text{is defined as the length causing 100% diversion. Hence,} \\ \text{by putting } \frac{Q_{D}}{Q_{S}} = 1.0 \text{ in Eq. (4.25)}$

$$L_{m_{1}} = \frac{y_{c}}{[0.51-0.41 \text{ Log (D/S)}]}$$
 (4.26)

For a constant D/S, Eq. (4.25) is valid for $\frac{L}{y_c} \leq \frac{L_{m_1}}{y_c}$ and for all $\frac{L}{y_c} > \frac{L_{m_1}}{y_c}$ the $\frac{Q_D}{Q_S}$ will obviously be unity.

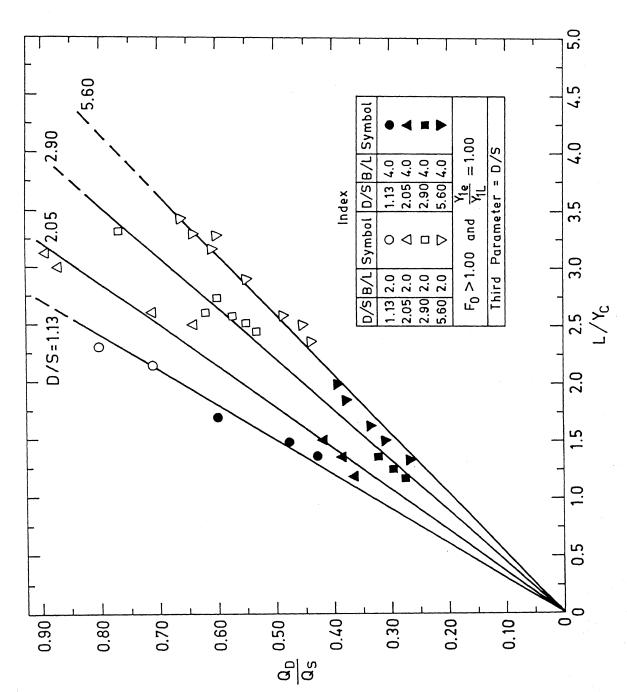
4.3.3 $\frac{Q_D}{Q_S}$ in Bl Flows

For Bl flows the variation of $\frac{Q_D}{Q_S}$ with $\frac{L}{y_c}$ by taking D/S as third parameter is shown in Fig. 4.11. Four values of D/S in each of the two sets B/L =2.0 and 4.0

respectively are plotted in this figure. The value of $\frac{B}{y_0}$ in all the data was in the range 6.98-15.38. It is seen that $\frac{B}{L}$ has no effect over $\frac{Q_D}{Q_S}$ for a given D/S while $\frac{Q_D}{Q_S}$ increases linearly with $\frac{L}{y_c}$. Also, $\frac{B}{y_0}$ has no distinct effect over the diversion ratio. The trend is consistent for all the four D/S values tested. Similar to Al flows, in this case also the variation of Q_D/Q_S with L/y_c is linear and can be expressed by Eq. 4.25, replacing m_1 by m_2 .

The slope m_2 is a function of D/S as seen in Fig. 4.11. The variation of m_2^* with D/S for Bl flows is also shown in Fig. 4.12, from which m_2 can be expressed as

$$m_2 = 0.36 - 0.26 \text{ Log (D/S)}$$
 (4.27)



Variation of Diversion Ratio in Super-critical Approach Flows (B1 Type). Fig. 4.11.

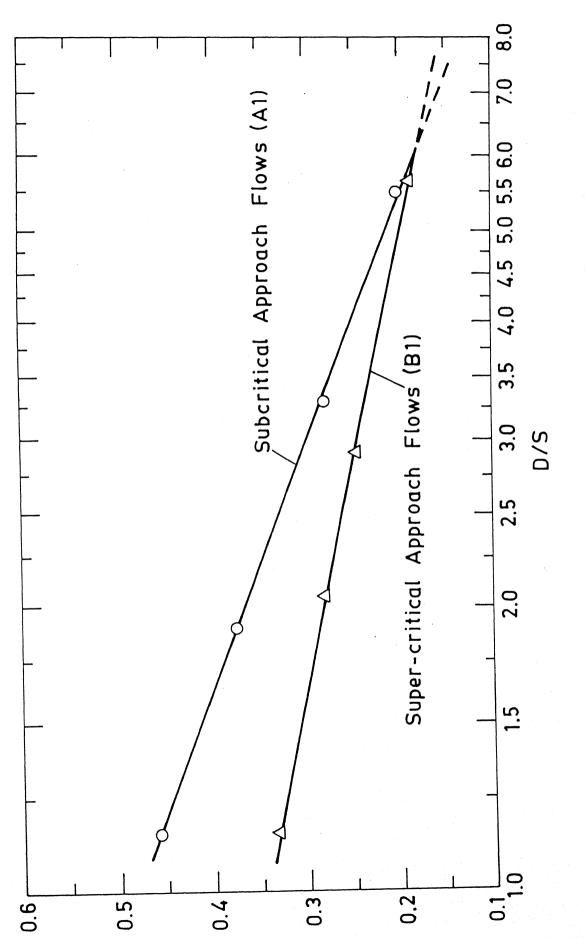


Fig. 4.12. Relation of m with D/S.

Combining Eqs. (4.23) and (4.27)

$$\frac{Q_{D}}{Q_{S}} = [0.36 - 0.26 \text{ Log } (D/S)] \frac{1}{Y_{C}}$$
 (4.28)

Further the minimum length L_{m_2} in Bl flows can be represented \not as

$$L_{m_2} = \frac{y_c}{[0.36-0.26 \text{ Log}(D/S)]}$$
 (4.29)

As in AI flows, for a constant D/S, Eq.(4.28) is valid till $\frac{L}{y_{c}} \leq \frac{L_{m_{2}}}{y_{c}} \text{ and for all } \frac{L}{y_{c}} > \frac{L_{m_{2}}}{y_{c}}, Q_{D}/Q_{S} \text{ will be unity.}$ It is observed that for a given $\frac{L}{y_{c}}$ and D/S, the diversion ratio is higher in Al flows than in Bl flows.

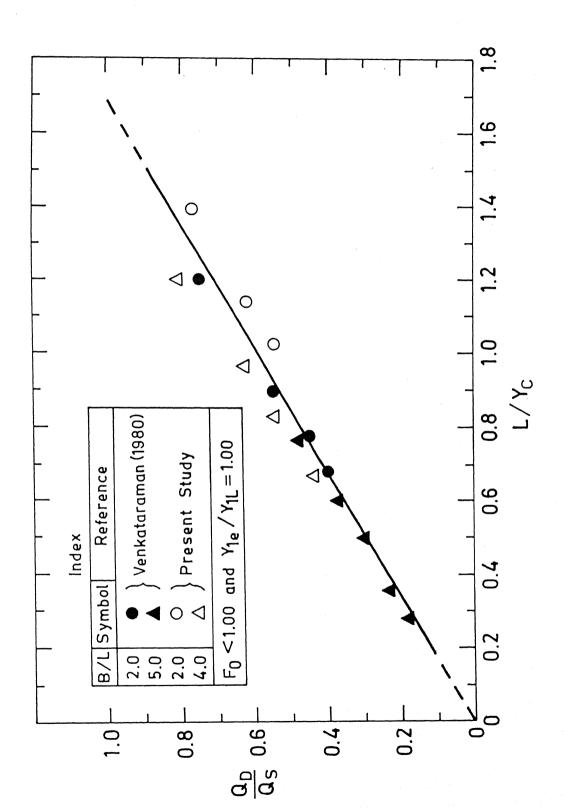
* In Fig. 4.12, m=m₁ (for Al flows) and m=m₂ (for Bl flows). 4.3.4 $\frac{Q_D}{Q_S}$ in Al flows over a Slot:

For Al flows over a slot the variation of $\frac{Q_D}{Q_S}$ with

 $\frac{L}{Y_C}$ is shown in Fig. 4.13. The experimental data of the present study for the two sets B/L = 2.0 and 4.0 along with the experimental data from Venkataraman (4) for B/L = 2.0 and 5.0 are plotted in this Figure. It is seen that $\frac{B}{L}$ does not affect the diversion ratio distinctly. Diversion ratio varies linearly with $\frac{L}{Y_C}$ and can be expressed as

$$\frac{Q_{D}}{Q_{S}} = 0.5883 \left(\frac{L}{y_{c}} \right) \tag{4.30}$$

From this equation for Al flows over a slot, $\frac{L_m}{y_c}=1.7$. The Eq.(4.30) is valid for $\frac{L}{y_c} \leq \frac{L_m}{y_c}$ and for all values of



Variation of Diversion Ratio for a Slot in Sub-critical Approach Flows (A1 Type). Fig. 4.13.

 $\frac{L}{y_c}$ > $\frac{L_m}{y_c}$ the diversion ratio will be unity, where L_m = minimum length of the slot required for 100% diversion.

4.4 Energy Loss Over the Rack:

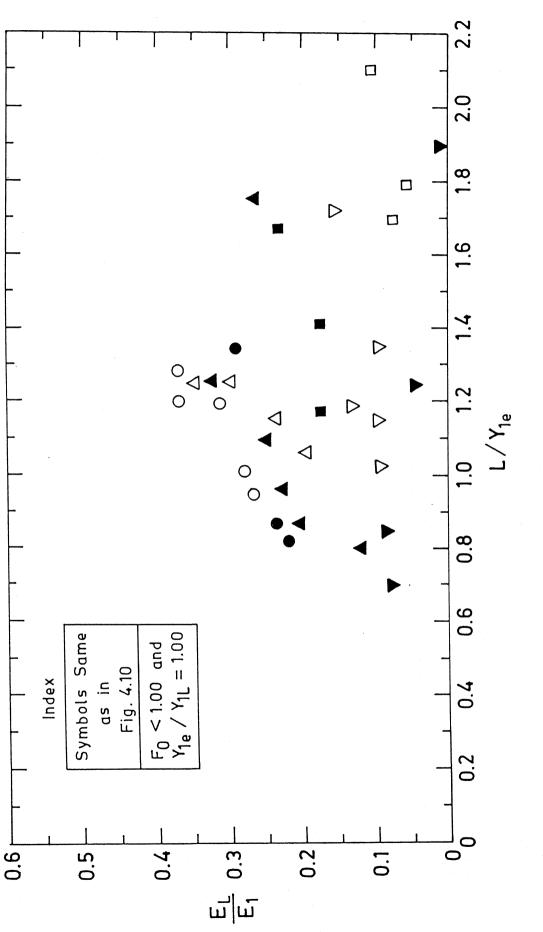
4.4.1 <u>Introduction</u>:

For determining the energy loss E_L over the rack, the specific energy at the inlet to the rack E_1 was defined as $E_1 = y_{1e} + \frac{V_1^2}{2g}$ by ignoring the correction for curvilinear flow over this section. Thus the energy loss over the horizontal rack can be approximated without serious error as

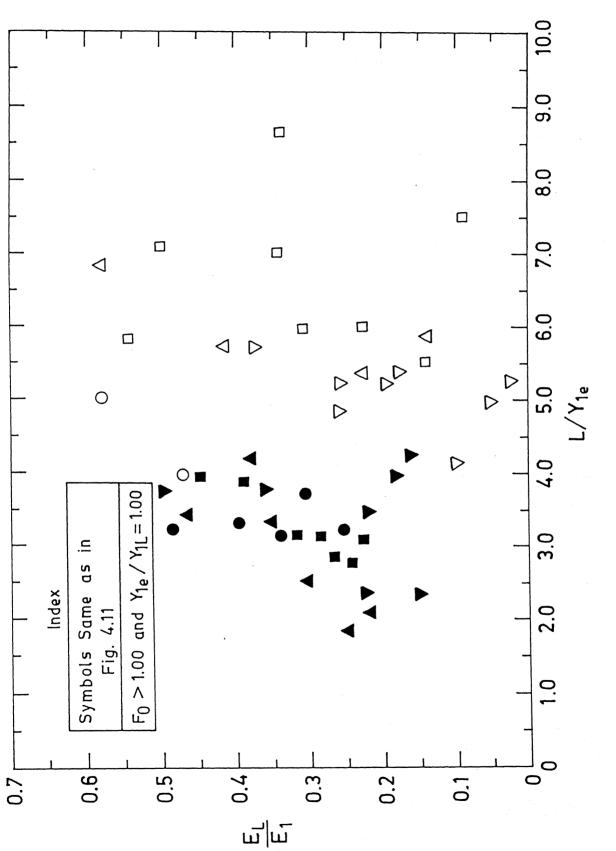
$$E_{L} = E_{1} - E_{2} = (y_{1e} + \frac{v_{1}^{2}}{2q}) - (y_{2e} + \frac{v_{2}^{2}}{2q})$$
 (4.31)

where suffix 2 represents the conditions at section 2. It is common in spatially varied flow analysis (for example Mostkow (3)) to assume the energy loss over the rack as negligibly small. As such, a study was made to find out the order of magnitude of the energy loss in the present investigation.

Plots of $\frac{E_L}{E_1}$ vs $\frac{L}{y_{1e}}$ for Al and Bl flows are shown in Figs. 4.14 and 4.15 respectively. It is seen that in both these flows there is considerable energy loss even though there is no direct correlation with $\frac{L}{y_{1e}}$. The average value of $\frac{E_L}{E_1}$ in Al flows is around 15% while it is about 30% in Bl flows. Also it was found that $\frac{E_L}{E_1}$ is not correlated with F_L in both Al and Bl flows.



Variation of Energy Loss Over the Rack in Subcritical Approach Flows (A1 Type) Fig. 4.14.



Variation of Energy Loss Over the Rack in Supercritical Approach Flows (B1 Type). Fig. 4.15.

In a simple model
$$E_L$$
 was defined as
$$E_L = K \frac{V_1^2}{2g} \eqno(4.32)$$

where K is the coefficient of energy loss. While an average value of K was obtained as 0.4 in both Al and Bl flows, there was considerable scatter and no distinct correlation with either F_1 or $L/y_{l\,e}$ could be obtained.

. In another model the energy slope $\mathbf{S}_{e} = \mathbf{E}_{\tilde{\mathbf{L}}}/\mathbf{L}$ was expressed as

$$S_e = fn (B,L, y_{le}, D, S)$$
 (4.33)

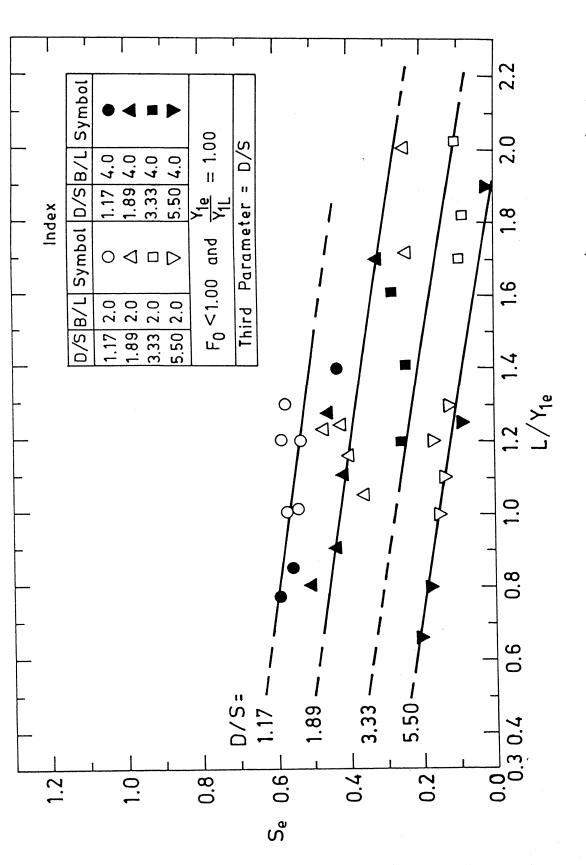
Groups of dimensionless variables affecting the variation of S_{Δ} can be written as

$$S_e = fn \left(\frac{L}{y_{1e}}, \frac{D}{S}, \frac{B}{L}\right)$$
 (4.34)

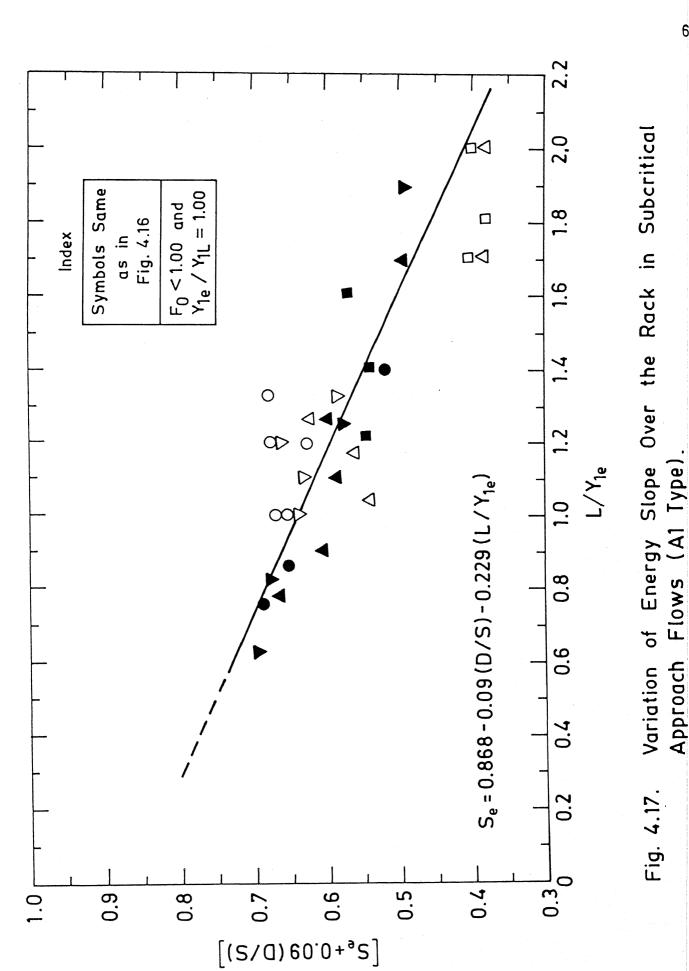
The variation of $S_{\rm e}$ with the parameters as in Eq. (4.34) is analysed separately for Al and Bl flows.

4.4.2 S_e in Al flows:

For Al flows the variation of S_e with $\frac{L}{y_{le}}$ by taking D/S as the third parameter is shown in Fig. 4.16. Four values of D/S in each of the two sets B/L = 2.0 and 4.0 respectively are plotted in this figure. It is seen that for a given D/S there is no effect of B/L and the value of S_e decreases with $\frac{L}{y_{le}}$. The trend is consistent for all the four D/S values tested. The variation of S_e for a constant $\frac{L}{y_{le}}$ was found to be related by a linear relation within the range of D/S values tested (viz, D/S=1.17 to 5.50) as



D/S in Relation of Energy Slope with L/Y_{le} and Subcritical Approach Flows (A1 Type). Fig. 4.16.



$$S_{Q} = 0.785 - 0.09 (D/S)$$
 (4.35)

Using this the best fit relation for the experimental data on Al flows was obtained as

$$S_e = 0.868-0.09 (D/S)-0.229 (L/y_{1e})$$
 (4.36)

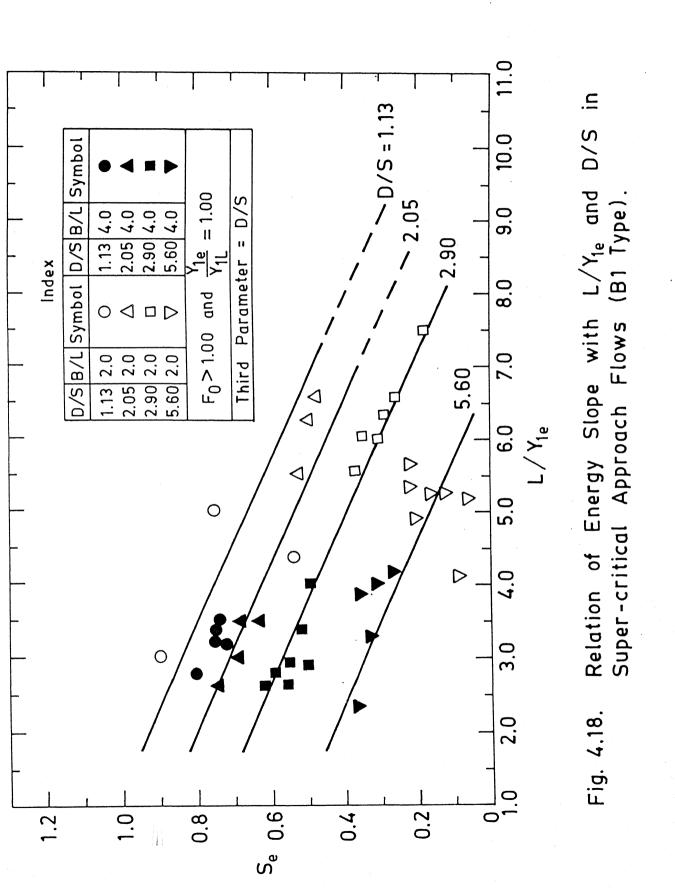
This is shown in Fig. 4.17 where $[S_e + 0.09 \text{ (D/S)}]$ is plotted against $\frac{L}{y_{le}}$ and all the data on Al flows are plotted. Eq. (4.36) is also shown in this Fig. The maximum scatter of the data was found to be \pm 15% and the average scatter was about 5%. Hence, this equation can satisfactorily be used for the estimation of the energy slope in Al flows over lengitudinal bar bottom—racks.

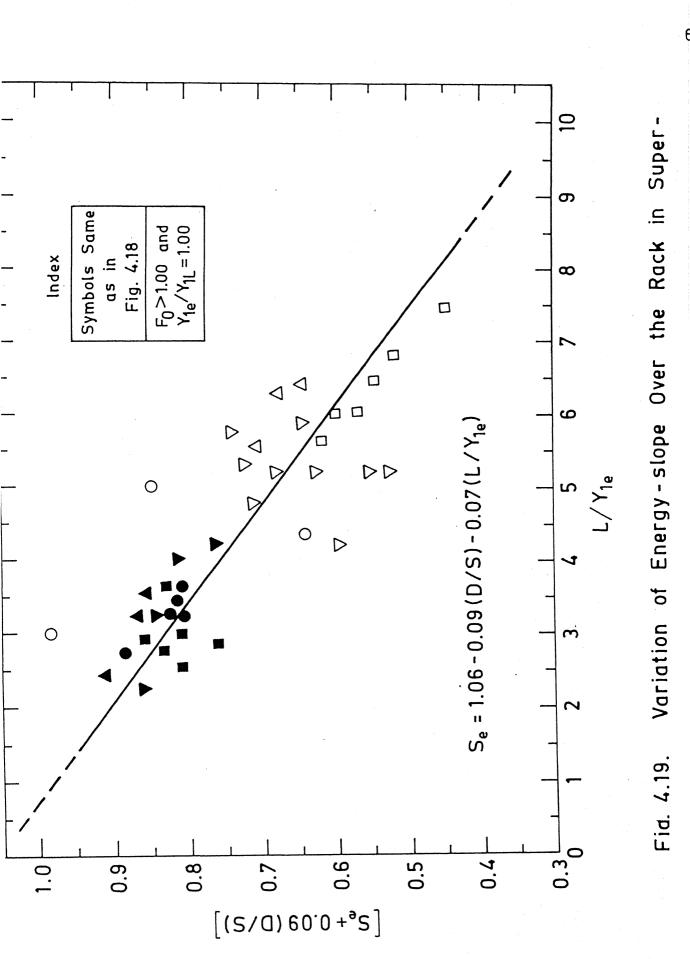
4.4.3 $\frac{S_e}{e}$ in Bl flows:

For Bl flows the variation of S_e with $\frac{L}{y_{le}}$ by taking D/S as the third parameter is shown in Fig. 4.18. Four values of D/S in each of the two sets B/L=2.0 and 4.0 respectively are plotted in this figure. It is noted that for a given D/S there is no effect of B/L and the value of S_e decreases with $\frac{L}{y_{le}}$. The trend is consistent for all the four D/S values tested. The variation of S_e for a constant $\frac{L}{y_{le}}$ was found to be related by a linear relation as

$$S_{e} = 1.01 - 0.09 (D/S)$$
 (4.37)

within the range of D/S values tested (viz, D/S = 1.13 to 5.60). The best fit relation for the experimental data on Bl flows was obtained as





$$S_e = 1.06-0.09 (D/S) -0.075 (L/y_{le})$$
 (4.38)

This is shown in Fig. 4.19 where $[S_e+0.09 \ (D/S)]$ is plotted against L/y_{le} and all the data on B1 flows are plotted. Eq. (4.38) is also shown. The maximum scatter of data is about 20% while the average scatter is roughly 8%. Hence, the equation (4.38) can satisfactorily be used for the estimation of the energy slope in B1 flows.

It is interesting to see that the coefficient of D/S in both the Eqns. (4.36) and (4.38) is same at 0.09. The energy slope, Se is smaller in Al flows, where the approach flow was subcritical, when compared to Bl flows. The range of parameters F_0 , F_1 , F_2 and L/y_{le} used in the study are shown in Table 4.1.

Table 4.1 Range of Parameters used in the Study of $S_{f e}$

Type of flow	F _o	$F_1 = \frac{V_1}{Vgy_{le}}$	$F_{2} = \frac{V_{2}}{\sqrt{gy_{2e}}}$	L/y _{le}
Al	0.60-0.85	1.1 - 1.5	1.1-1.45	0.67-2.10
Bl	1.3 -5.4	1.6 - 6.1	4.8-6.5	2.0-8.0

It is obvious from the Table 4.1 that in Al flows, the inlet Froud number F_1 varies in a very small range (1.1-1.5) and the range of flows F_1 through F_2 is also small. However, in Bl flow high Froude numbers as much as 6.5 were encountered

and account for higher energy losses. The Eqs. (4.36) and (4.38) must be considered as only approximate relationship. However, they underscore the magnitude of E_L and their use is definitely an improvement over the assumption of zero energy loss.

4.4.4 Energy loss in A3 Flows:

The analysis of all experimental data on A3 flows shows that the percentage energy loss ($\frac{E_L}{E_1}$) for most of the data lies within 2 to 4%. Also, the energy slope (S_e) for mighty percent of data ranged from 0.05 to 0.15. The range of energy loss and the pertinent parameters of the flow observed in the study of A3 flows are shown in Table 4.2.

Table 4.2 Range of Energy Loss Parameters in A3 Flows:

Parameters	etatu, set se usak iransi kitandik iribidi melekanggi rangka tapin basatu sahi		ange
	Min.	Max	Average
F_			
<u>-L</u> %	0.0	10.0	3.5
s _e	0.0	0.22	0.09
L/y _{le}	0.15	0.90	0.40
Sb	0.10	0.55	0.25

The range of E_L/E_1 shown in Table 4.2 is quite small and no distinct variation of $\frac{E_L}{E_1}$ or S_e could be observed with and other parameters. More over, it is clear from

^yle

Table 4.2 that the energy loss $\frac{E_L}{E_1}$ as well as energy slope S_e are quite small. An average value for whole the data observed is given in the table with a view to show that majority of data were well within 2 to 4% energy loss.

Hence, for the analysis of A3 flows, the energy loss over the rack for $S_b \leq 0.55$ can be taken as negligible for practical purposes.

4.5 Water Surface Profile Calculations:

In view of the above analysis, it is obvious that the energy loss over the rack particularly in Al and Bl flows can not be neglected. As such, Equations (2.4) and (2.12) suggested by Mostkow for water surface profile calculations along the rack by assuming constant specific energy all along it, are not justified to use.

The original equation of SVF with decreasing discharge for a rectangular, prismatic and horizontal channel by taking kinetic energy correction factor $\alpha=1.0$, can be represented as

$$\frac{dy}{dx} = \frac{-S_e - \frac{Q_D q_{\frac{1}{2}}}{gB^2 y^2}}{1 - \frac{Q_D^2}{gB^2 y^3}}$$

$$(4.39)$$

where S_e = Energy slope over rack; Q_D = Diverted flow through the rack;

and $q_* = discharge per unit length of the rack and can be defined as$

$$q_* = \frac{Q_D}{L} = C_d B \in \sqrt{2gE_o} = Constant$$
 (4.40)

 $C_{\rm d}$ can be calculated from equation (4.12) or (4.17) depending upon the type of flow Al or Bl respectively.

 $S_{\rm e}$ can be calculated from equation (4.36) or (4.38) depending upon the type of flow.

Then, the Eq. (4.39), after substituting the values of S_e and q_{*} , can be solved by a suitable numerical technique to obtain the water surface profile over the rack. Since, the energy loss in A3 flows, is negligibly small, Mostkow equations (2.4) and 2.12) can be used for water surface profile determination in this particular case.

CHAPTER V

CONCLUSIONS AND RECOMMENDATIONS

5.1 <u>Conclusions</u>:

A detailed experimental study has been made on the hydraulic behaviour of horizontal longitudinal bar bottom-racks, made of circular bars, in Al, A3 and Bl flows. Based on the study the following conclusions are drawn.

- 1. The variation of the limiting inlet depth ratio $\frac{y_{1L}}{y_c}$ has been studied for Al and Bl flows separately. In Al flows it is found that $\frac{y_{1L}}{y_c}$ varies with the opening area ratio and is not affected by B/L ratio of the rack, while in Bl flows $\frac{y_{1L}}{y_c}$ depends upon the Froude number of approach flow F_0 as well as \in .
- 2. A coefficient of discharge C_d is defined as $C_d = \frac{Q_D}{BL \in \sqrt{2g}E_o}$ Variation of C_d has been studied in Al,A3 and Bl flows separately. It is observed that C_d is a function of $\frac{V_o^2}{2gE_o}$ and D/S ratio of the rack in all the three types of flows studied. The effect of B/L on C_d is found to be insignificant. The effect of the flow parameter $\frac{V_o^2}{2gE_o}$ is found to be negligible in Al flows while it has a pronounced effect in Bl flows. The best fit Eqs. (4.12), (4.15) and (4.17) have been obtained for

estimation of C_d in Al,A3 and Bl flows respectively. It is found that the value of C_d in Bl flows for a given flow and rack parameter is higher than the corresponding value in Al flows. Also, C_d in A3 flows is higher than that in Al flows. Al and A3 flow over the limiting case of a rack (viz, a slot) are also studied.

- 3. The diversion ratio $\frac{Q_D}{Q_S}$ is found to be a function of $\frac{L}{Y_C}$ and $\frac{D}{S}$ for Al and Bl flows. It is observed that the value of $\frac{Q_D}{Q_S}$ is higher in Al flows than for corresponding value in Bl flows. The variation of the diversion ratio in Al and Bl flows are expressed by Eqs (4.25) and (4.28) respectively. The minimum length of the rack required for the whole diversion of the incoming flow has also been obtained from these equations.
- 4. For a slot in Al flows the diversion ratio is related with $\frac{L}{y_c}$ by a simple equation (Eq. 4.30).
- 5. An attempt has been made for the determination of the energy loss over the rack. An average value of percentage energy loss with respect to inlet specific energy is determined as 15% and 30% in Al and Bl flows respectively. It is also observed that energy loss in A3 flows can be taken as essentially zero. The variation of S_e has been studied with $\frac{L}{Y_{1e}}$ and $\frac{D}{S}$ for both Al and Bl flows separately. It is found that the value of S_e in Bl flows is higher than the corresponding value in Al

- flows. Best fit equations (4.36) and (4.38) have been determined for estimating the energy slope $S_{\rm e}$ in Al and Bl flows separately.
- equations for water surface profile determination, based on the assumption of zero energy loss seems to be erroneous. As such, using the energy slope Se calculated from corresponding equations obtained in the present study, in the original equation of SVF with decreasing discharge and solving it by any suitable numerical method, is the suggested approach for the determination of water surface profile over the rack. However the Mostkow equations can be used for determining water surface profiles in A3 flows without much error because of the negligible energy loss in this flow case.
- 7. Information of this study is useful in the design of trench weir intakes. A simple fortran program has been given in appendix II for determining the length of such trench weirs and compared with their original recommended design.

5.2 Recommendations:

Based on the literature review and the present study, the following further studies on this topic are recommended.

- 1. Inclined lognitudinal bar bottom-racks need to be studied.
- The study could be extended to the perforated plate bottom-racks also.
- 3. Study could be extended for other shapes of bars namely Rectangular, stream lined etc to obtain efficient and economical bar geometry.
- 4. A more detailed study is needed for energy loss determination over the rack.

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7	34.0	0.15	.075	1	0.00421	0.00370	0.054	980.0	0.013	27.8	0.85 SHIP
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ເກ	0.48	0.15	.075	1.17	PL900°C	0.00421	0.072	0.048	970.0	a • L 7	90-758-0
9	0.48	0.15	. 975	-	0.00914	0,00453	0.088	840.0	0-036	27.8	40-348-0
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.	0,48	0.15	.075	100	0.00467	0.00350	0.056	850.0	0.012	27.2	0.85E-105
N	0.48	0.15	.075	4	0.00669	0.00410	990.0	0.044	0.050	27.8	0.858-06
2	0,48	0.15	0.75		97600.0	0.00559	0.094	0,084	060-0	27.8	0.85E-06
gerd gerd	0.48	0.15	.075	-	0,01119	0.00665	0.108	0.102	0.1.0	27.8	0.852.106
2	0.48	0.15	.075	-	0.01250	0.00702	0.128	9710	0.132	27.8	90-358
13	0.36	0.15	0.75	€ 80°	0.00820	0.00370	0.094	090.0	0-042	3.72	SOLUTE.
*	0.36	0.15	.075	1.89	89800.0	0.60370	060.0	090.0	0.040	27.8	3.65E-u6
5	0.30	0.15	75	1,89	0.00610	60800*0	990.0	0.044	0.020	27.8	90-958-0
91	0,36	0.15	.075	1.89	0.01085	0.00400	960°0	990.0	0-041	3.72	0.85E-10f
5	0.36	0.15	.075	5 α ••	0,01240	0.00410	0,104	0.072	0.050	8.72	90-250-0
8	0.36	0.15	. c75	7.89	0.00485	0,00291	0.058	0.038	0.014	27.8	90-350.0
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20	0.36	0.15	.075	1,89	0,01568	0,00534	0,132	0,115	0.124	27.8	90-352-0
21	0.24	0.15	. 075	3,33	0.00248	0.00177	0.038	0,025	0.010	22.0	90-356*0

											-
22	0.24	15	.075	3,33	0,06391	0.0000	0.048	0.035	0.014	22.0	0.450105
23	0.24	51.0	• 075	3,33	0.00537	0.00227	0.000	0.042	070-0	0.62	0.000105
24	0.24	0,15	.075	3,33	0.60577	0.00237	0.004	0.044	0-022	22.6	ない口になって
25	0.24	51.0	910.	3,33	6,00765	0.00340	0,092	0,044	880-0	22.0	0.958-06
26	0.24	0,15	\$7.0	3,33	0.00920	0.00400	0.128	0.120	0-120	22.6	90-256.0
27	0.24	0.15	.075	3,33	0.01189	0.00486	0.186	0.174	0-174	0.62	0.955-06
28	0.24	5	370	3,33	0.01348	0.00534	0,224	0,268	0.208	22.0	0.95E=06
29	0.16	0.15	375	5,50	0.00505	0.00147	0.056	0.045	0.030	22.0	0.955-06
30	0.16	51.5	.075	5,50	0.01027	0.00197	860.0	0,071	0.054	22.0	0.05E-06
31	0.16	5.	.075	95.	6020000	0.00171	0.076	950.0	0.038	22.0	90-356.0
32	0.16	0.15	.075	5,50	0.00926	0.60184	0.088	990.0	0.050	22.0	0.95E-106
33	0.16	0,15	675	5.50	0.00861	0.00177	980*0	0.002	0.50.0	22.0	90m356-0
34	0.16	5.0	5.075	5,50	0.01477	0.00340	0,192	0.184	0.184	22.0	0.00 0.00 0.00
35	0,16	0.15	.075	5.50	0,01198	0.00279	0.138	0,129	0-138	22.0	6.95E=06
36	0,16	0.15	.075	5.50	0,01381	0.00322	0,180	0.174	0.176	22.0	ひょうという
37	0.16	0.15	.075	5.50	09600*0	0.00214	0.092	0.012	0.078	22.0	0.25E-06
38	0,16	0.15	.075	5.50	0,01052	6.06239	0.108	560.0	0.100	22,0	90-356.0
39	0.16	0.15	.075	5,50	6.01682	0.00340	0,235	0.224	0-224	0.68	90-356-0
40	0,16	2	960.	00.00	0.00552	0,00076	0.064	0.046	0.040	24.0	0.91E-06
41	0.16	51.1	.038	2.30	0,00283	6,00062	0.040	0.0	070-0	24.0	0.918-06
42	0.16	0.15	.038	5,50	0,00159	0.00055	0.030	0.020	0-010	24.0	90-316-0
43	0.10	6.15	.038	5,50	0.00720	0.00000	0.078	950.0	0.050	24.0	0.91E-06
*	0.10	0,15	.038	5.50	86600.0	0,00131	0.134	971.0	0.130	24.0	90-316-0
45	0.16	0.15	960.	5.50	0.01331	0,00165	0.206	951.0	0.196	24.0	C.91L-06
97	0.16	0.15	.038	5.50	0.01514	0.00184	0.232	0,232	0-232	24.0	0.918-06

										-	
11	Same of the same o	51.0	ာ င	0 0 0	0.01568	0.00184	0.246	9.7.0	956-0	24.C	C. VIETOR
20	6,24	5	°€	3,33	0,00140	0.00076	0.026	815.0	0-014	5	0.956-06
67	0,24	5.5	* 0.38	S. 8. 8. 8. 8. 8. 8. 8. 8. 8. 8. 8. 8. 8.	0,00222	0.00084	0.034	423.0	910-0	22.0	0.95E=06
50	0,24	0,15	.038	3,33	0.00271	06000*0	0.040	170.0	810-0	22.6	90*345*O
15	0,24	5	.038	3,33	0.00330	0.00097	0.044	0.031	0-022	22.0	0.95E=U6
52	0.24	5.5	9€0*	3,33	0,00476	0,00145	0.080	870.0	0-u18	22.0	0.95E=06
23	0,24	5.5	.038	3,33	0,00628	0.00184	0.120	0.112	0-112	22.0	90-756-0
ν. 44	0.24	0.15	.038	3,3	0.00824	0.00221	0.172	0.164	0-164	22.6	0.95E=06
55		5	.038	ج ج پ	0.01051	0.00267	0.230	0.220	0.220	22.0	0.95E=06
56	36.0	5	° 038	1,89	0.00204	0,00111	0.034	0.022	010-0	24.0	0.51L=Ch
57	36.0	0.15	*038	* * * *	0.00568	0.00153	0.062	0,042	0.030	24.6	0.91E-06
သ	36	S	3£0°	1.89	0.00145	6,00111	0.030	0.018	0.00	7.52	0.91E=06
5.9	0.36	15	\$£9.*	7) CC	0,00310	0,00136	0.044	0.030	07.0-0	24.0	0,93E=06
09	0.36	61.5	. 038	200	0,06472	0,60153	0.058	0.040	0-030	20.02	0.91E=06
61	0.36	5	.038	.89	98900*0	0.00171	0.070	0.046	0.040	24.6	0.915-06
79	0.36	い さ つ	.038	1,89	0,00381	0,00142	0.050	0.034	170-0	J. 12	0.931.06
63	0.36	0.15	\$60.	. 89	0,00769	0.00207	0.082	940.0	6.089	0° VZ	0.91E=06
49	6,36	5	860*	1.89	19690*0	0,00271	0.130	0,126	0-130	24.6	0.915-06
65	0.36	5	*038	£ 0.0	0.01204	0,00322	0.178	0.168	0-172	24.0	0.91E-06
99	0.36	5	.038	1.89	0.01378	0.00350	0.208	0.200	0.200	24.0	0.91E-0£
19	0.48	0.15	.038	-	6790000	0.00190	990.0	\$ 0.0 ° 0	0-036	22.0	90-325-0
89	0.48	0.15	\$60*	1.	60700.0	6.0000	0.074	0.048	6-042	22.0	90-356-0
69	0.48	0.15	.038		0,00300	0,00153	0.044	0.128	¥10-0	22.6	0.95E-ué
7.0	0.48	6.15	.038	1.17	0,00795	0.00247	£30.0	97.0.0	980-0	22.6	0.95E=06
-	0.48	0.15	.038	1.17	0.01018	0.00313	0,134	0.132	0-134	22.0	90-356-0

							78				
72	0.48	16: 	9E0.		0,01228	0.00370	0.178	0,170	6-172	22.0	0.956.06
73	0,48	公	.038	1.00	0.01384	0.00400	0,212	0.204	0.204	22.0	U.95E-06
74	0.48	£7	.038		0.01522	0,00415	0.240	0.232	0-232	22.0	7. VAT-10F
75		0.15	.038		19200	0.00218	0,038	0.022	0.010	22,0	0.752-06
76	Jahren Ja	5	.038	<u></u>	0.00458	0.00251	0.054	0.034	0.018	22.0	0.95E=0A
77	3	0.15	.038	0000	0.00624	0.00271	0.004	0.040	67070	22.6	0.956-06
78	00	5	000	3.0	0.00159	0.00159	0.028	910.0	0-000	22.0	0.956-06
7.9	-	444	360	000	6,00363	0.00236	0.046	970.0	0.013	22.0	0.95E=cf
Üä		6.15	360	00.0	0.00761	0.00390	0.078	0.04A	010-0	22.6	0.958=06
20	3	0.15	.038	30°C	0,00911	0.00487	960*0	950.0	960-0	22,0	0.95E104
82		5.0	8E)*	Se*0	0,01055	0.00565	0,110	0.114	0.11.4	22.0	97-356°0
8	-	27.	869.	00.0	0.01309	6,00762	0.164	0.160	0-160	22.0	0.358-06
© ©		0,15	350.	99.0	0.00296	96200*0	0.038	6.02A	0-002	22.0	0.95E=U6
85	Š	0.15	.075	000	0,00578	0.00442	0.000	980.0	0.008	22.0	0.95E=06
86		2 3	.075	00.0	0.00776	0.00476	0.072	970.0	070-0	22,0	30.05E-0.0
87	00.	0.15	0.075	00.0	0.00920	0.00499	0.082	0,052	970-0	22.0	0.958-06
α α	30	0.15	.075	00.0	0.01071	0.00637	0.094	C. (16.4	0-074	22.0	0.95E.=06
68	00.1	0.15	.075	00.0	0.01267	0.00888	0.108	0.042	960-0	22.0	0.95E=06
36	700	0.15	\$ 0.75	00.0	0,01416	0.00974	0.118	860.0	850-0	22.0	0.958-66
16	1.00	0.15	• 075	00.0	0,01507	0.01043	0.126	0,116	0-120	20.02	90-756.0
92	0.49	09.0	.170	644 644 644	0.04660	0.04560	090.0	0.051	0-001	30.0	0.816-06
66	0,49	09.0	300	1.13	0.09100	0.07370	0.080	970.0	810-0	36.0	0,818-06
76	0.49	09*0	.300	1.13	0.09510	0.05830	0.05R	0.058	0-036	30.0	0.816-06
95	0.34	09.0	300	2.05	0.05670	0.05160	0.052	0.052	9.00.0	29.0	6.81E-06
96	0.34	09.0	.300	2,05	0.08020	0.05160	0.054	0.054	0-025	0.62	0.818-06

	2000	3 · 0
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122	0.10	99*	150	19.5	0.05346	0.01799	0,052	9.0.0	0.034	24.6	
123	0.10	59.0	051.	w.	0.07396	0.01980	0.066	6.04	0.050	24.0	0.01010
125	0.16	09.0	.150	5	0.07310	0,01943	0.002	940.0	0-056	24.0	2.91E=0A
125	0.27		051	2,90	0,05133	0.02508	0.054	0.044	870-0	7. 27	S. S. C.
126	0.27	09.0	.150	ુ ે વ	0,03549	0.02408	0.048	0.038	0.016	24.0	\$0.00 \$0.00
127	0.27	09*0	.150	2,90	0.06388	0,02528	0.064	0.054	0-038	20.05	0.918-06
128	0.27	09.0	.150	2.30	0.06771	0.02412	0.058	950.0	0-042	24.0	0.918-06
129	0,27	09*0	150	2,30	0.07370	0.02316	0.056	0.054	97000	24.0	0.916-06
129	0.27	09*3	.150	2.90	0.07891	6.02278	0.000	0.052	0-045	24.0	6.91E=06
130	0.27	09*	.150	2,90	0.08056	0.02241	950.0	0.055	0-046	20.0	901916.0
132	0,34	0.0	.150	20.0	0.04350	0.02727	0.050	570°0	270-0	7.4.	AU-816.0
133	0,34	09.0	.150	2,05	0.05816	0.02431	0.048	0.040	0-030	7.42	0.918-06
-	50	09.0	150	2,05	0.06774	0.02241	0.050	0.050	C*0-0	0.62	30-316.0
135	£ 0	09.0	150	2.05	0,07486	0.03084	0.070	0.000	250-0	24.0	0.0
136	0.34	00.0	V:	2,05	0.07968	0.02982	0.072	0.072	0.050	7. 77	
137	0.34	0.60	.150	2.05	0.08194	6.03392	0.086	0.040	0-052	24.0	2012 TO
138	0,49	09.0	.150	£ .	0.05146	0.03084	0.054	970.0	970-0	22.0	90-826-0
139	0,49	09*0	15.	~	0.06103	0.02854	0.052	0,048	0.033	22.0	0.956.06
***	0.49	09.0	.150	1.13	0.06686	0.02684	0.052	940.0	0.033	22.0	0.956-06
142	0.49	09*0	.150	1.13	0,07253	0.02586	0,058	0.50	0-037	22.0	2.95E=u6
143	0,49	09.0	.150		0,07851	0.02469	0.054	0.054	0.047	22.0	0.00 0.00 0.00 0.00
EXPS.	144 TO	146 FUR	VELOCITY	TY PROFILE	LE UMLY.						

TABLE IN (DEPWED DATA)

	Signal designation and designa	S/U	111111111111111111111111111111111111111	(VO**2/20E0)	D. C. Company of the	00/08	92	11/16	./// 10	um Alberten Gille Mar litter Alter etter jätet prin äner anne-
n. 477	7 0	G / C			A Sept.				ם. ד. כ	ou ou ou ou ou ou ou ou ou ou ou ou ou o
The Court State St	0.48	1.17	0.75	0.222	895*0	0.458	U.528	C. 45	1.19	7.81E+05
N	0,43	dung anny	0.71	0.203	16.594	0.879	0.073		2,08	0.33F+05
m	87.0	-	0.74	0.214	0.574	0.476	0.581	ω Ω	<u>.</u> .	0.735 +05
-*	0.48	1	0.74	0.214	0.555	0,373	0.558	67.0	66*0	0
S.	84.0		0.74	0,216	0.580	0.624	0.592	1.27	1,50	0.538+05
٥	0.48	1.17	0.75	0.217	0,565	0,496	0.548	1.04	1.29	0.72E+05
7	0.48	1.17	0,79	0,236	0.573	0.367	0,550	0.16	0000	0,111,00
ထ	0.48	-	0.75	0.220	0.547	0.750	0.517	1.62	1.0.1	0,3/8405
6	8.4.0	1.17	0.84	0.261	0.574	0.613	0.537	2.29	1.70	0.525+05
	0.48	-	0.72	0,206	6.079	0,573	0.263	6 F 3	68.0	0,775+05
epad epad	0.48	1.17	19.0	0.184	0.764	0.594	0,150	5.	6.0	20+2880
7.	6.48	1.17	0.58	0.144	0.759	0.562	0.165	P . C	(9° c	0.988405
Ţ	0.36	1.89	0.61	0,155	0.518	0.451	0.457	errei errei errei	1,25	0.648405
	0.36	1,89	89.0	0.190	0,618	0.426	0,430	1.07	1.25	0.688403
in H	0.36	1.89	11.0	0.226	685*0	9.506	0.210	1.36	1.70	0.438+05
16	0.36	1.89	0.78	0,232	0.630	0,368	0,389	6.9	- A	0,855+05
11	0.36	1.89	0.79	0,236	0.619	0.331	0,357	50.0	70.	0.978405
18	0.36	7.80	0.74	0.215	0.598	0.601	0.234	1.58	1.97	0.385+05
10	0.36	1.89	19.0	0.184	0.752	0,369	0.273	91.0	19.0	0,112+06
20	0.36	1,89	0.70	0,195	0.736	0.341	0,232	0.12	69.0	0.128+00
21	0.24	3,33	0.71	0.203	6.679	0.714	0.345	2.47	3,00	0.17E+05

22	0.24	3,33	67.0	0.239	0,060	0.511	7-60°0	1.63	2,14	0.215+05
23	0.24	ω ω ω	0.70	0.232	080°0	0.424	740.0	1.99	2.70	0.38E+08
1 6	0.24	, e. e. e.	0.76	0,223	069.0	0.411	0.091	4 4 4	-	204705
, c	0.24	3.33	0.58	0,145	098.0	0.445	1.01.0	1.17	68.0	504E45.0
250	0.24	3,33	0,43	0.084	\$68°0	0,435	0.121	1.03	0.63	0,4309,0
12	0.24	3,33	0,32	0.047	0.920	0.409	0.092	0.07	0.43	SCALE C
233	0.24	3,33	0.27	0.035	0,927	0,396	0.081	00*0	0,36	0.955405
23	0.16	5,50	18.0	0.248	119.0	0,292	0.151	1.04	1.67	0.305405
30	0.16	50°	0.71	0,202	0.704	0.192	0,145	0.26	1.00	0.725+03
(*	0.16	5.5	0.72	0,206	0,693	0.241	0.119	1,23	1.34	C0+405.0
32	0.16	5.50	0.76	0,222	0.685	0,198	0.142	1.03	***	0.535+03
33	0.16	0.00 0.00	0,73	0,209	\$79.0	0.206	0.178	80.1	1.21	0.605405
34	0.16	5,50	0.37	0.005	0.941	0.230	0.079	0,75	0.41	0.10E+00
35	97.0	o in	05.0	0.110	0.898	0,233	0.007	0.87	0,58	0.945405
36	0.16	5.50	0,38	690.0	0.918	0.233	0.054	61.0	0.43	CO+4/0.0
37	0.16	r.	0.74	0,215	0.784	0,221	0.184	(in * 1	*	0.688405
38	91.0	o v	0.63	0,166	583.0	0.228	FOT . 0	\$ 6 ° 0	67.0	0.728+05
39	91.0	5.00	0.31	0.047	0.859	0.202	790.0	60.0	0.33	0,125400
40	0,16	36. C	9,73	0,208	0.672	0,138	0.175	6,13	78.0	0.4408+05
~	0.16	50.50	0.75	0.221	0.084	9.218	0.065	1.13	1,25	0.212+05
42	0.16	5.50	0,65	0.175	0.726	0,347	-0.003	1,06	٠ د د د	0,128405
43	0.16	5.50	0.70	0,198	0.727	0.126	0,201	0.01	19.0	0.535+05
4	0.16	5.50	0.43	980.0	0,858	0,131	#00.0°	67*0	0.30	0.738+05
45	0.16	5.50	0.30	0.044	0.891	0,124	0,065	0,40	0.19	0.938+05
46	0.16	5.50	0.29	0.040	0.937	9,121	0,059	0,37	0.10	0.118+00

0.115400	+0+286.0	0.105+05	0.138+05	0.238705	0.335403	0.445405	0.535+05	0.745405	0.15E+05	0.425+05	0.115+05	0.238+05	0.355+05	0.472+05	0.285+05	0.50F+05	0,715+05	0.835+05	0.10E+00	0.444	0.505+05	0.218+05	0.502+03	0.71E+05
0.15	2°0°	1.50	1,39	~ C	0.48	0,33	0.23	0.17	1.70	68.0	2.03	1,25	0.0	0.82	2	0.57	0.30	0.22	5	0.85	0.78	de la company de	0,19	0.28
0,36	1.01	1.53	1.17	1.02	0,00	0,07	95.0	1.47	1.41	17.0	1.17	1.07	0,01	90.0	6, 33	0.38	05.0	0.43	65.0	0.07	[c. 5]	60.1	70.0	44.0
0.054	0,340	0,283	0.241	0.247	0.110	0.095	0.071	0.061	0.317	0.269	0.548	0.455	0.425	0.498	0.424	-0.013	0.075	0.045	0.127	0.530	765.0	0.402	0.143	0.139
0.117	0,545	0.380	0,334	0,294	0.303	0.292	0.268	9,254	0.544	0.269	0.763	0.439	0,324	0.269	0.372	0.269	0.230	0.267	0.254	0,302	0.283	0.510	0,311	0.307
\$16°0	0.706	0.674	0.673	0.681	0.814	0.864	0.878	0.921	109.0	0,599	0.657	0.645	0.631	0.040	0.628	0,723	008*0	0.827	0,837	0.541	0.544	0.548	0.640	0.682
0,036	0,201	0,221	0,206	0.224	160.0	0,049	0.029	0.020	0,193	0.235	0,150	0,203	0,205	0.211	0.209	0,195	0.088	0,055	0.046	0.238	0.219	0,193	0,194	0.089
0.27	0.71	0.75	0.72	0.70	0,45	0.32	0.25	0.20	69.0	0.78	65.0	0.71	0.72	0,73	0.73	0.70	0.44	0.34	0.31	0.79	0.75	69*0	69*0	0.44
5.50	3,33	3,33	3,33	3,33	3,33	3,33	3,33	3,33	1.89	1,89	1.89	4.89	1.89	1.89	1.89	7.89	1.89	1.89	1.89	1.11		1.17	1.17	
0.16	0.24	0.24	0.24	0.24	0.24	0.24	0.24	0.24	0.36	0.36	0.36	96.0	0.36	0.36	0,36	0.36	0.36	0.36	0,36	0.48	0.48	0.48	0.48	0.48
47	48	50	51	52	53	54	55	26	2.1	28	59	9	61	62	63	\$ 9	65	99	29	89	69	70	7	72

73	6	7	0,35	0.057	0.711	0.301	0.11	6.43	72.0	0.905+03
74	8.0	Anni, Anni,	0.30	0.044	0.710	0.289	0.137	05.5	0.13	0.978+05
75	0.48	denn,	0,28	0.037	060.0	0.273	0.123	15.0	0	0.115+00
76	5		0,75	0.220	0.396	0.833	1.050	1.20	1.70	0.135+05
7.1	9	The state of the s	0.78	0.232	0.880	0.548	0.724	0.42	1.10	0.325+05
78	5.	Topological States of the Control of	0.82	0,252	0.372	0.434	166.0	0.07	* 6 ° 0	0.445+05
79	•	96.0	0.72	0,206	0.424	1.000	1,010	1,53	 	0.118+05
80	0	3	0.78	0.234	0.386	0.650	0,946	96.0		0.258+05
 &	3	0	0.74	0,216	0.495	0,512	0.524	64.0	0,59	0.538+05
82	5	30.0	0,65	0,175	0,573	0.535	0.420	0,52	0.39	0.648405
83	5	00.0	0.55	0,130	0.614	0.536	0.400	6,47	0.33	0.748405
œ	00.1	0000	0.42	0.081	190.0	0,537	0.318	U. 4.	0,23	0.925+05
85	1.00	00.0	0.85	0,265	0,356	1,000	1,025	L of	2,29	0.218405
G S	00.1	00.00	± 00° €	0,259	0,312	0.705	0.284	7,0	5.03	0,415+05
	Ser	20.0	0.25	0.267	70°0	0.613	0.525	1,16	1.63	0.548405
<u>ග</u> ස	00	00.0	0,83	0.258	0,301	0.542	0,493	1,03	•	9.658+05
္	3	0.00	61.0	0,238	0.364	505.0	500.0	6,03		0.758+05
Š	9	00.0	0.70	0,224	0.477	001.0	0.472	69.0	0.82	0.895+05
Grad		000	0,74	0.217	#0S*0	6.688	695.0	0.17	0.77	0.995+00
2		30.0	0.72	0.205	0.526	0.692	0.411	41.0	0.65	0.115+00
<u> </u>	0.49		1.69	0.587	0,555	1.000	0.986	03.4	3,33	0.908+05
Ö	67*0	13	2,14	969*0	0.370	0.810	0.434	97.7	3° 0°	0,195+00
. c	0,40	1.13	3,62	898*0	0.227	0,613	0.849	2,19	5.17	0.20E+00
9 6	0.34	2.05	2,54	0.764	- - - - -	0,899	0.104	3.10	5.77	0.128+00
67	0.34	2.02	3,40	0.853	0,315	0,643	0.520	94.7	5.56	0.175+00

0.333 0.874 0.826 0.364 0.537 0.364 0.597 0.591 0.330 0.263 0.263 0.279 0.558 0.172 0.359 0.459 0.556 0.360 0.408 0.560 0.860 0.507 0.507 0.673 0.105 0.653 0.653 0.105	0.856 0.835 0.867 0.946 0.928 0.936	3 2 8 8 8 9 8 9 9 9 9 9 9 9 9 9 9 9 9 9 9	2,05 2,05 2,96
0.558 0.558 0.558 0.539 0.526 0.625 0.625 0.673	0.835 0.860 0.928 0.928 0.785		2 8 9
0.768 0.558 0.539 0.539 0.526 0.625 0.735 0.673	0.846 0.846 0.912 0.928 0.801		2,89
0.591 0.558 0.526 0.735 0.625 0.740	0.846 0.912 0.928 0.936 0.801		
0.558 0.539 0.526 0.735 0.625 0.730	0.928 0.928 0.936 0.801		(5) (5) (5)
0.539 0.526 0.735 0.625 0.760 0.673	0.928 0.936 0.801 0.785		4.56
0.526 0.735 0.625 0.780 0.673	0.936 0.801 0.785		5.07
0.735 0.625 0.860 0.780 0.673	0.801		5.40
0.625 0.860 0.780 0.673	0,785		2.83
0.860 0.780 0.673			2,70
0,780	989*0		5.09
0,673	0.476		1,35
709.0	019.0		1.4
	699.0		2.01
0,645 0,650 0,216	679.0		1.92
0.610 0.553 0.180	0.703		2,17
0.561 0.485 0.200	0.745		2,42
0,511 0,448 0,293	0.803		2.86
0.476 0.436 0.229	0.842		3.26
0.574 0.439 0.081	0.713		2,23
0,630 0,615 0,029	0.647		1.91
0.820 0.582 0.358	965.0		1.72
0.654 0.406 0.259	0.742		2,40
0,601 0,378 0,311	0.795		2.78
0.576 0.309 0.597	0.803		2,86

123	0.16	5,61	2.40	0.742	0.640	0,337	0.328	10° 1	3°5°	0,986+05
124	0.16	5.61	2,32	0.729	0.641	0.268	0.240	1.30	2,3	-
125	0.16	5.61	2.52	0.760	0.010	0,266	0,358	Alemai Alemai	16.6	
126	0.27	2.90	2,18	0.703	0.552	0.489	0.562	5.00	(r) 4() 	0.045405
127	0.27	2,90	38.	0.617	6.639	619.0	0.400	2.13	3,95	0,655+05
128	0.27	2.90	2,10	0,688	0.525	0.396	#5. p. 0	1.43	2.78	0.125+00
129	0.27	7.90	2,58	0.769	0,452	0.356	0.457	H . 38	89.2	0.125+00
130	0.27	2.90	2,96	0,814	0.396	0.314	7.000	1 * 30	2.78	0,138+06
3.4	0.27	2,90	2.86	0.803	0.388	0.289	0.554	1.24	2.88	0.141.406
32	0.27	2,90	3,23	0.840	0,350	0.278	0.577	1,22	2,73	0.15F+06
133	0.34	2.05	2.07	0.682	0,508	0.627	0.550	5.0.	3.4	C. PUFFOS
134	0.34	2.05	2,94	0.812	0,355	0.418	098.0	1,52	3.75	0.115400
135	0.34	2,05	3,22	0.839	0.297	0,331	0.686	1.57	300	0.12F+00
136	0.34	2.05	2,15	0.698	0.472	0.412	0.552	57.1	2.50	0.14E+00
137	0.34	2.05	2,19	0.707	0.444	0.374	0.364	E 7 *	2.08	0.15E+00
138	0.34	2.05	1.73	0.590	0.540	0.414	0.372	7	\$ 8 °	0.15E+00
139	0.49	1.13	2.18	0.704	0.372	0.599	0.721	59.7	3.26	20-70-0
140	σ ₄ . Ω	1.13	2.74	0.789	967.9	0.168	0.711	1.47	3.15	2-11-0
141	0.49	€	3,00	0.818	0.258	0.401	0.653	0.5	3,26	0.125+00
142	0.49	1,13	2.76	0.792	0.252	0,357	0.571		3.00	30+35
143	0,49		3,33	0.847	0.214	0.314	\$ 0 R . 0	1,25	2.78	6-148+00
EXPS.144	144 TO 146	STAND	FOR VELOCIT	IY PROFILE	ONLY.					

APPENDIX II

The main part of the design of trench weirs includes that of Longitudinal Bar Bottom-Racks. The present study indicates that the following field parameters are required for the the design of such racks:

- (i) The total stream flow, QS
- (ii) The diverted flow through the rack , QD
- (iii) The width of the rack /channel , B
- (iv) The depths , YO and Yie
- and (v) The diameter of the bar ,D and spacing , S between the bars.

The spacing can be chosen on the basis of the size of the sediment present in the stream.

with the suggested correlations one can use the above parameters to calculate the length of the rack. A simple Fortran program has been developed and given on the next page. The length calculated from this program with the available data for BANU and PARAI trench weirs alongwith their recommended length is given in Table I

TABLE I Comparision of design lenths.

Weirs	Leng	th (m) ca	alculated		Length(m)	
	рА	present	method		provided	
BANU	6425 Ares 6224 6004 6460 5092 6080 6040	1 g 1	pot seur seur aper dan berr upp durp dem stam eine.	STATE AND WHITE PARTY SEALS AND THE	2.0	* 1996 West State
PARAI		1.5			2.0	

PROGRAM RACK

TRENCH WEIR -- RACK DESIGN

THE FOLLOWING PROGRAM CALCULATES THE LENGTH(L1) OF A BOTTOM RACK FOR WHICH APPROACH FLOW(QS), DIVERTED FLOW(QD) THROUGH RACK, YU, Y1e, DIAMETER(D) OF BARS, SPACING (S) BETWEEN THE BARS AND WIDTH(B) OF CHANNEL IS KNOWN. HERE YO IS DEPTH AT A DISTANCE '5Y1e'FROM U/S BRIUF RACK &Y1e IS U/S BRINK DEPTH.

REAL L,L1 READ(21,*) OS,QD,Y0,Y1e,D,S,B V0=QS/(B*Y0) E0=Y0+((QS*QS)/(19.62*B*B*Y0*Y0)) EPS=(S/(D+S))

THE OPEN AREA RATIO "EPS" HAS BEEN MULTIPLIED BY 0.45 BY CONSIDERING 10% REDUCTION DUE TO FRAME WORK AND 50% DUE TO CLOGGING TO GET "EPS1".

EPS1=0.45*EPS
F0=08/(B*3.132*(Y0**1.5))
YC=((05*QS/B*B*9.81)**(1.0/3.0))
DS=D/S
IF ((Y0.GT.YC).AND.(Y1e.LT.YC)) GO TO 50
IF((Y0.GT.YC).AND.(Y1e.GT.YC)) GD TO 100
CD=(ALOG(D/S)*0.36)-1.084*(Y0*Y0/(19.62*E0))+1.115
WRITE(22,7)
FORMAT(/,20X,'FLOW IS B1 TYPE')
WRITE(22,8)
FORMAT(/,20X,20('-'))
GU TO 150
CD=(ALOG(D/S)*0.20)-0.247*(V0*V0/(19.62*E0))+0.601
ARITE(22,10)
FORMAT(/,20X,'FLOW IS A1 TYPE')
WRITE(22,8)
GO TO 150
CD=(ALOG(D/S)*0.28)-((V0*V0/(19.62*E0))*0.565)+0.752
WRITE(22,8)
GO TO 150
L=QD/(EPS1*B*CD*(SQRT(19.62*E0)))

LENGTH, L IS INCREASED BY 10% TO GET DESIGN LENGTH , L1.

L1=1.1*L

WRITE(22,12) OS, OD, YO, D, S, B, CD, DS, YC, Y1e, EO, FO, EPS, L

FORMAT(/,10X, OS=',F7.3, 'CUMECS',/,10X, 'OD=',F7.3, 'CUMECS',

1 /,10X, Y0=',F6.3, 'METERS',/,10X, 'D=',F6.4, 'METERS',/,10X,

1 'S=',F6.4, 'METERS',/,10X, 'B=',F5.2, 'METERS',/,10X, 'CD=',F6.3,

1/,10X, 'D/S=',F6.3,/,10X, 'YC=',F6.3, 'METERS',/,10X, 'Y1e=',F6.3,'

1 METERS',/,10X, 'EO=',F6.3, 'MTRERS',/,10X, 'Y1e=',F6.3,'

1 THE RACK RECOMMENDED=',F5.1, 'METERS',/,20X,30('_'))

STOP

END